

A Holistic Approach to Addressing Halite Precipitation and Remediation Strategies in CO₂ Injection Wells

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Overview

- Halite risk during CO₂ storage
- Predicting halite deposition
- Effects of imbibition and gravity
- Injection rate and intermittency effects
- Washwater treatments
- Conclusions
- Acknowledgements

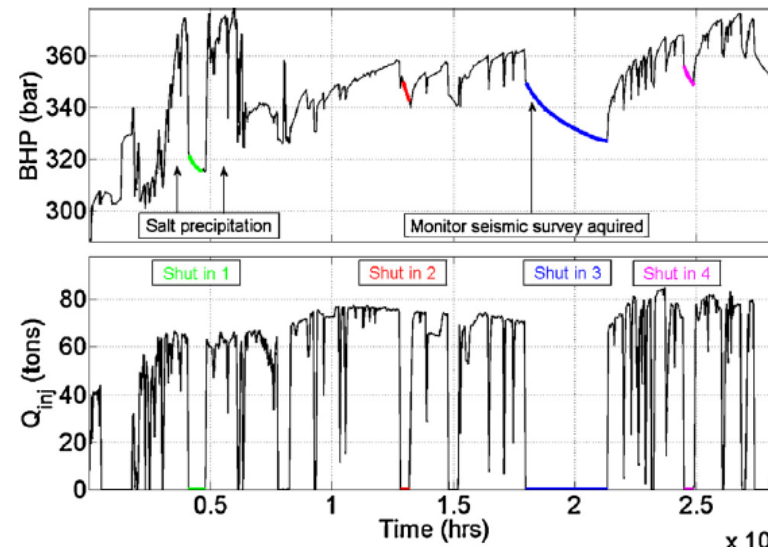
Halite Risk during CO₂ Storage

- Halite precipitation observed in Aquistore CO₂ injection well during shut in
- 340,000 mg/L formation brine
- Brine re-enters well during shut in:
 - Imbibition
 - Gravity
- Evaporation of brine causes increase in salinity to saturation
- Other minerals also precipitating?
- Could these cause more damage?

Solution		Precipitates			
	g/L		mmoles/L	g/L	cc/L
Na ⁺	87.7	Halite	3815.0	222.95	102.7
K ⁺	4.96	Sylvite	124.0	9.24	4.6
Ca ²⁺	32.5	CaCl ₂ ·2H ₂ O	809.3	118.98	64.3
Mg ⁺	1.70	MgCl ₂ ·6H ₂ O	70.0	14.23	9.1
Cl ⁻	203.0	Anhydrite	1.6	0.22	0.1
SO ₄ ²⁻	0.15	Calcite	0.4	0.04	<0.1
HCO ₃ ⁻	0.05	Total			180.9
Br ⁻	0.71				

Halite Risk during CO₂ Storage

- Downhole video tool shows effect of brine ingress into well and evaporation
- More deposits lower down in well
- Can this also occur in formation?
- Loss of injectivity also observed in Snøhvit, which was partially recovered by MEG/washwater treatments



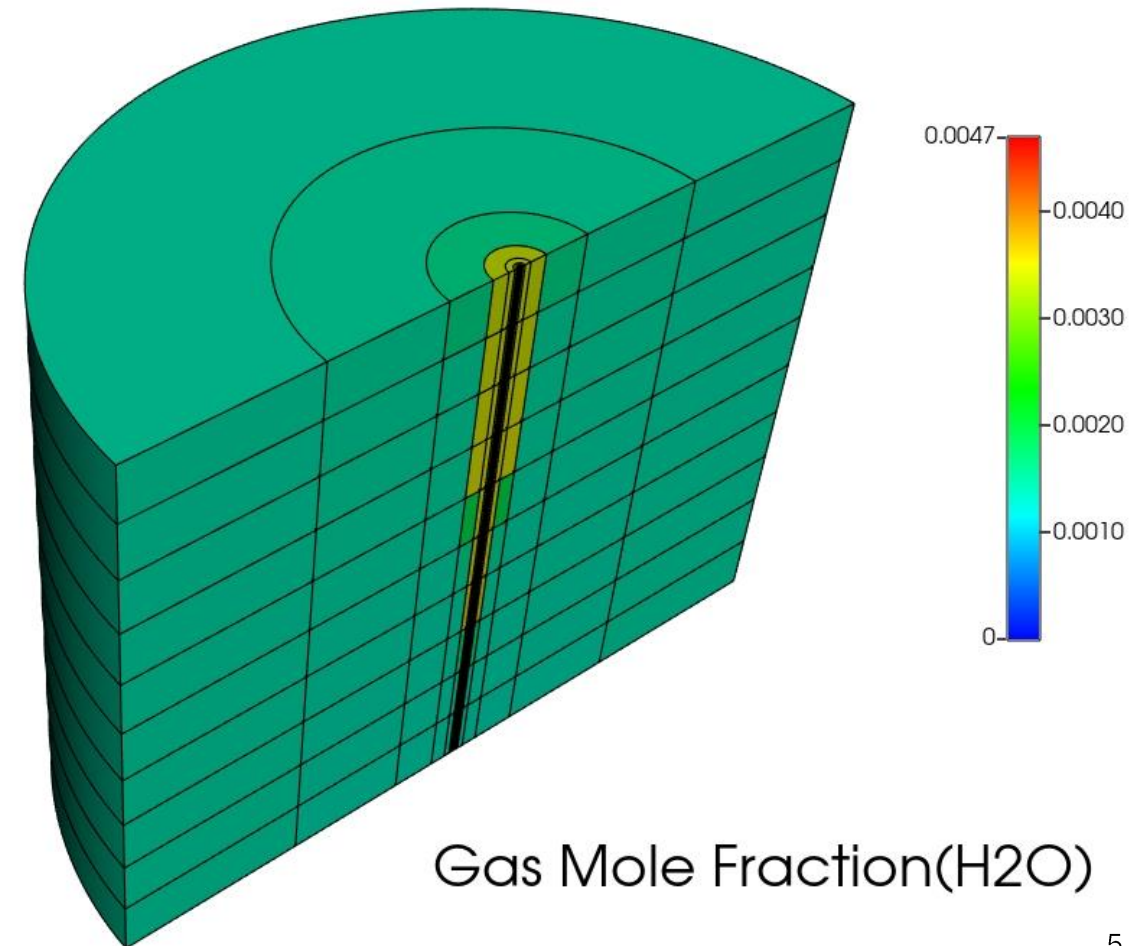
Grude *et al.* (2014)



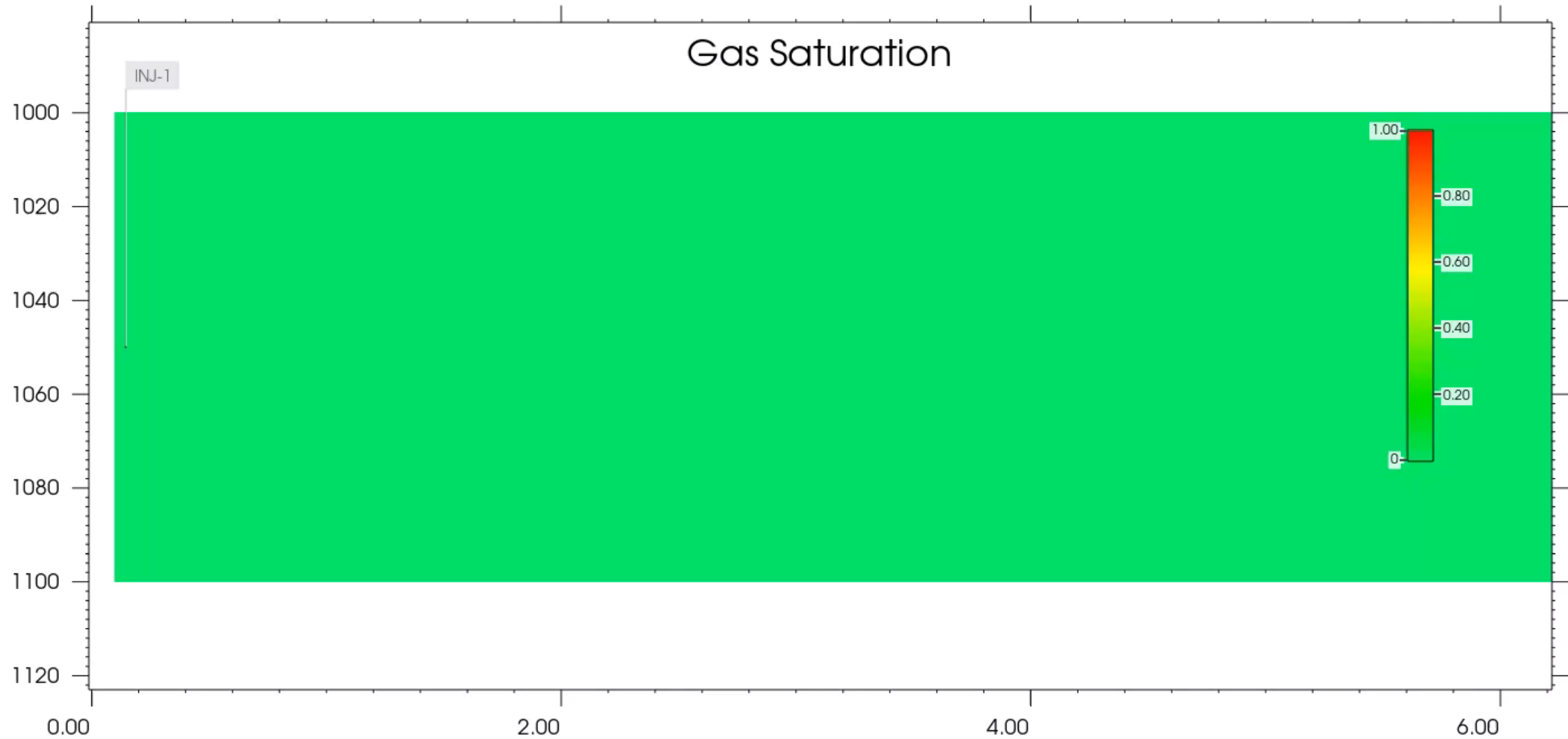
Talman *et al.* (2021)

Predicting Halite Deposition during CO₂ Storage

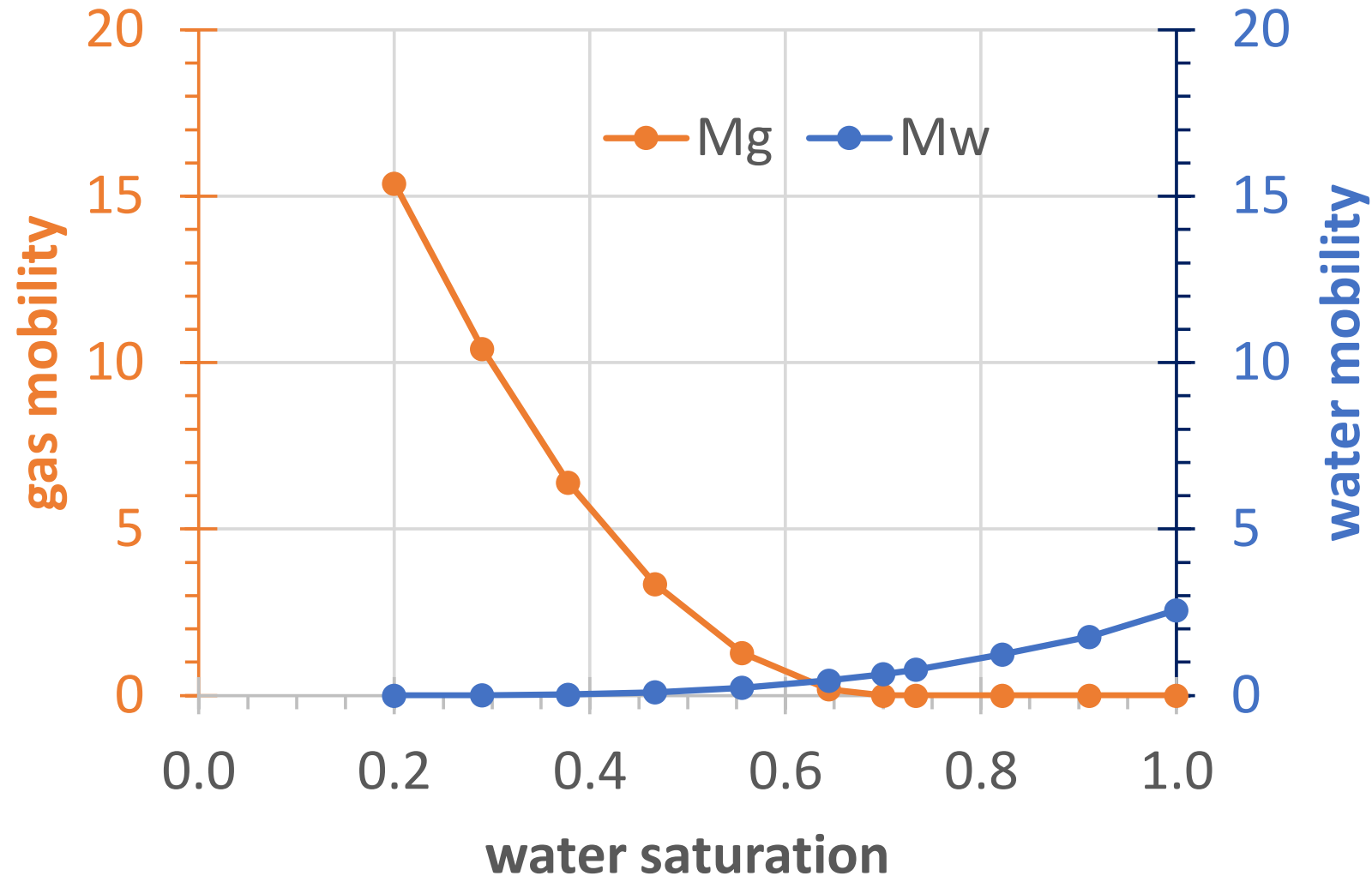
- Use 1D and 2D radial models of CO₂ injection into a saline aquifer
- Test impact of
 - Evaporation / no evaporation
 - Deposition / no deposition
 - Imbibition / no imbibition
 - Gravity (2D) / no gravity (1D)
- Calculate
 - Dry out zone
 - Porosity change
 - Injectivity change



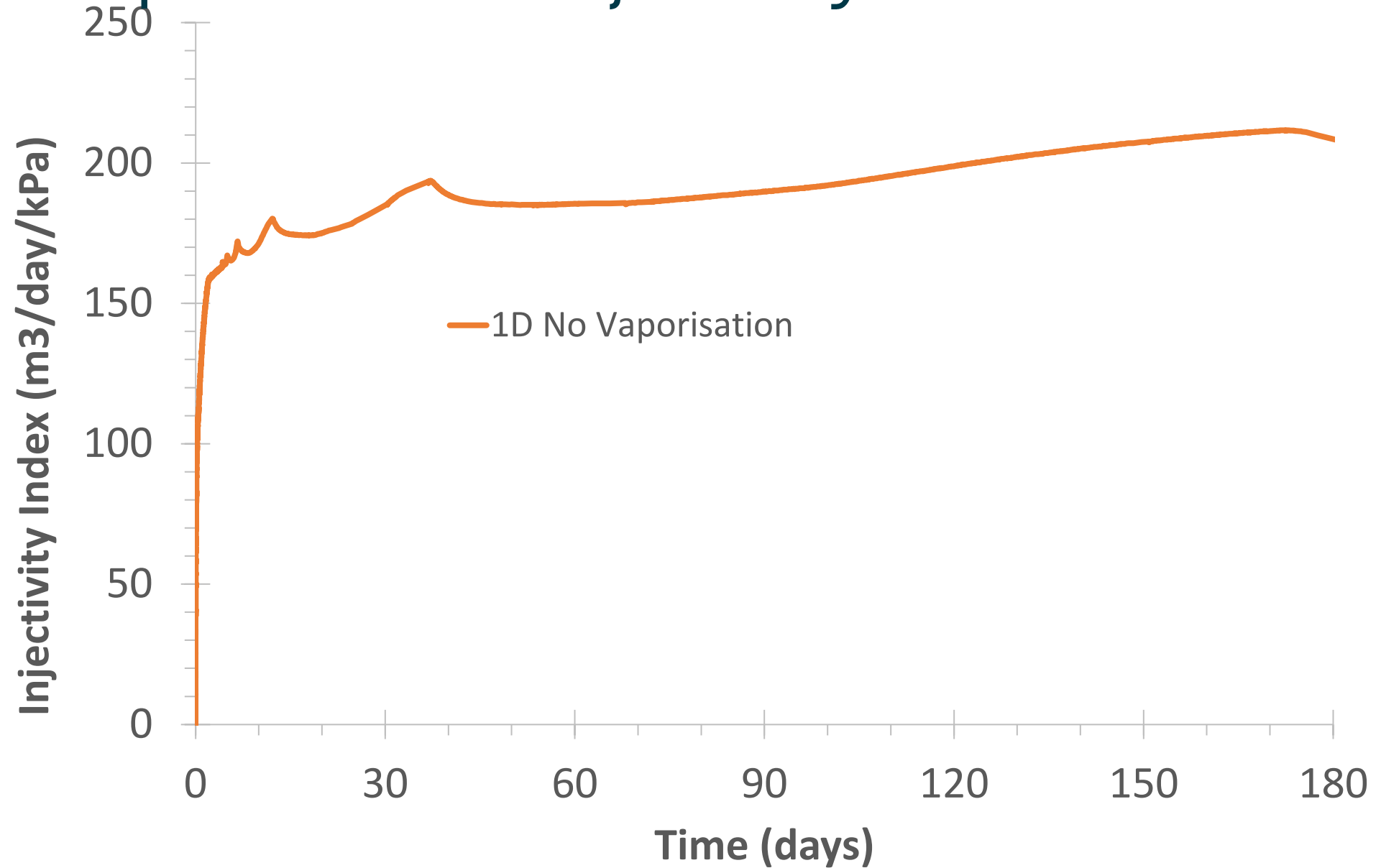
1D No Vaporisation - Gas Saturation



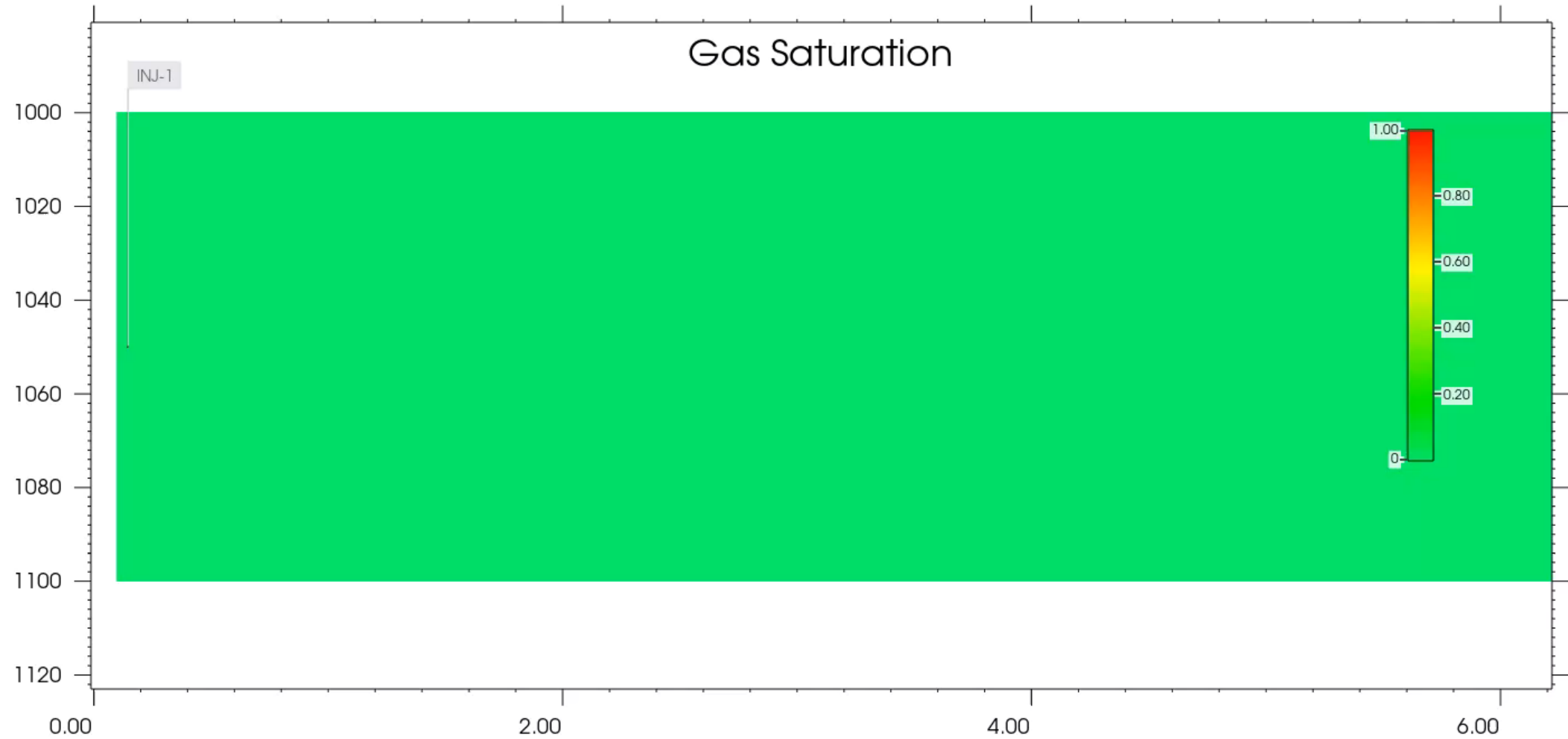
1D No Vaporisation – Mobilities



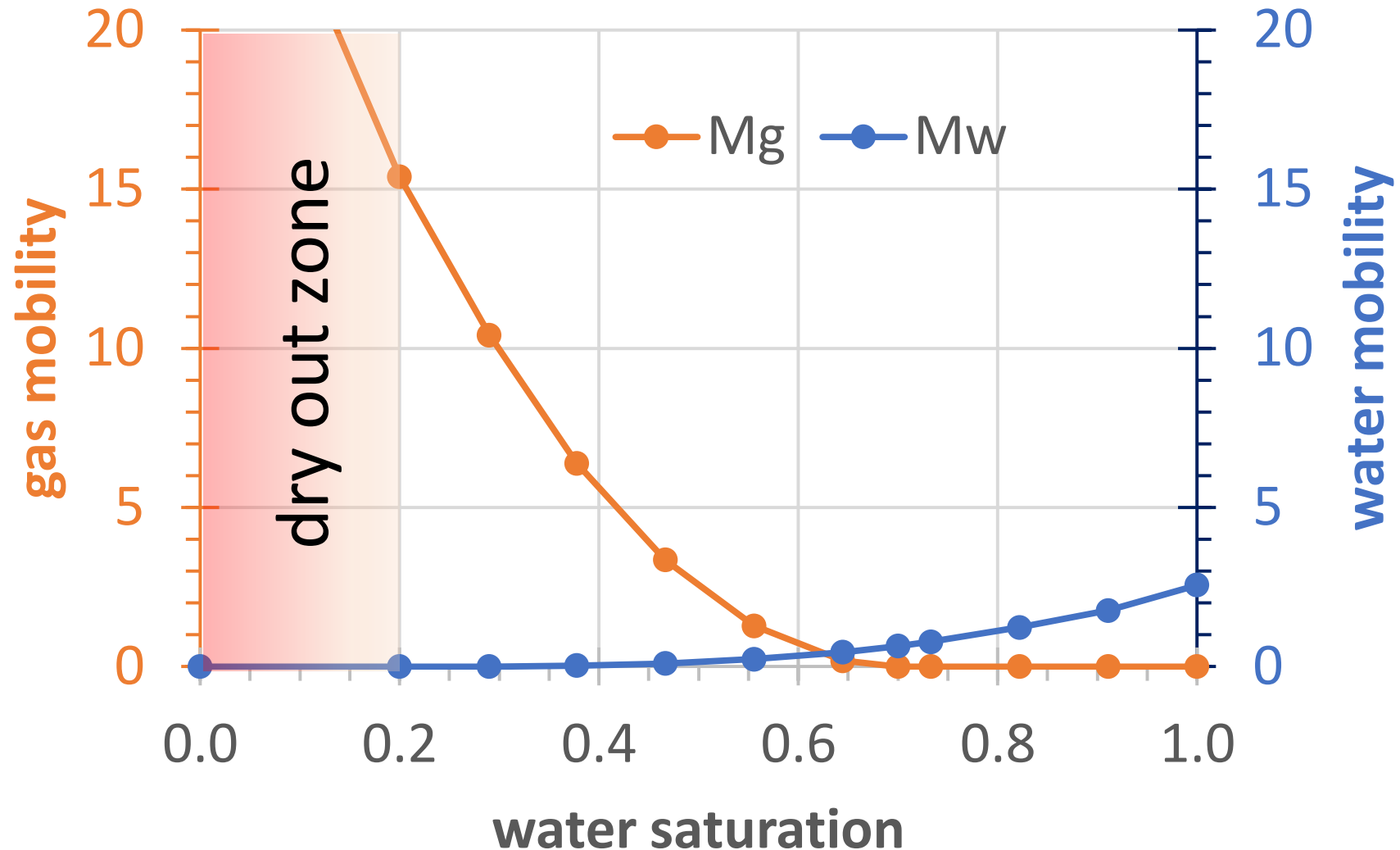
1D No Vaporisation – Injectivity Index



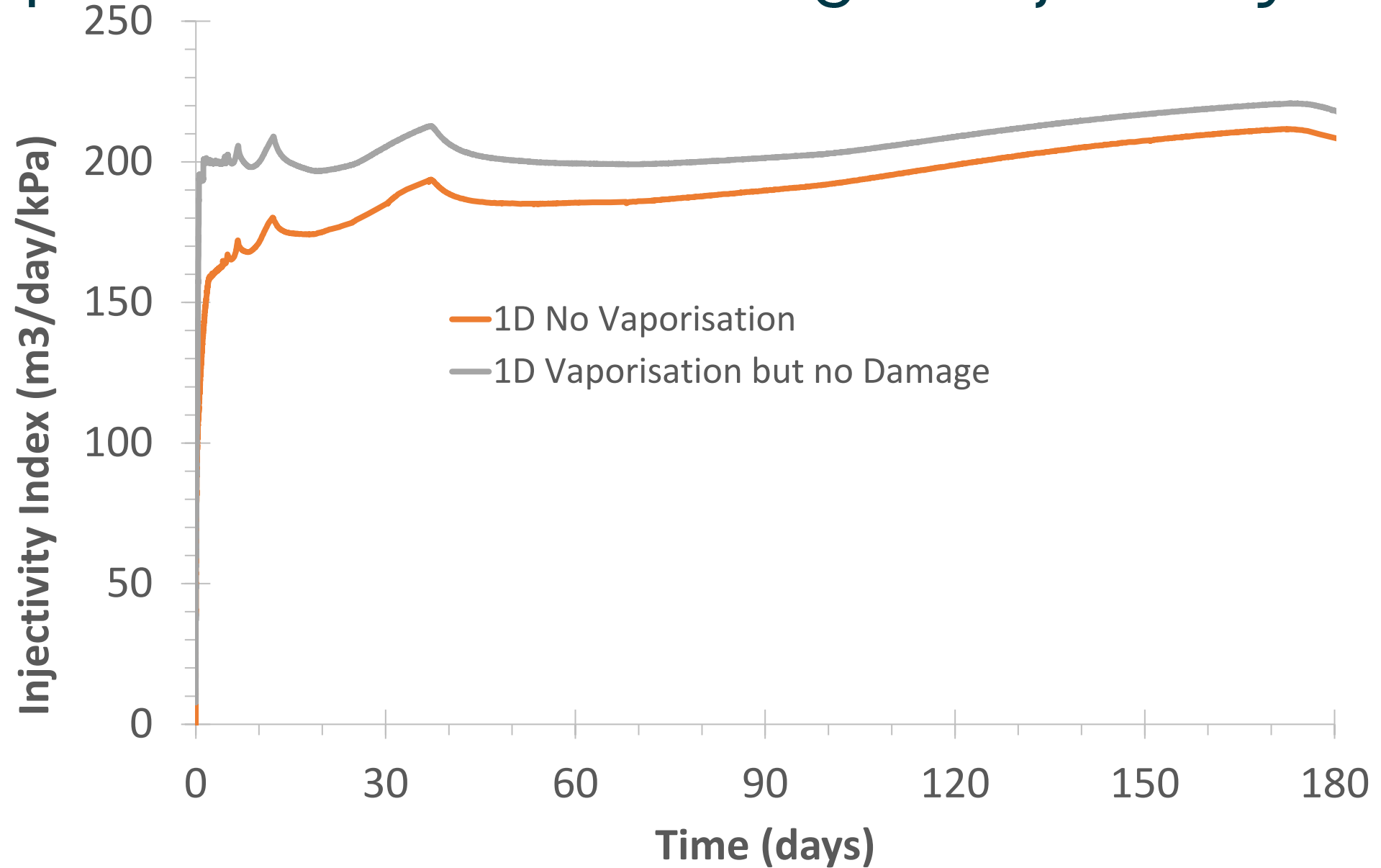
1D Vaporisation but no Damage - Gas Saturation



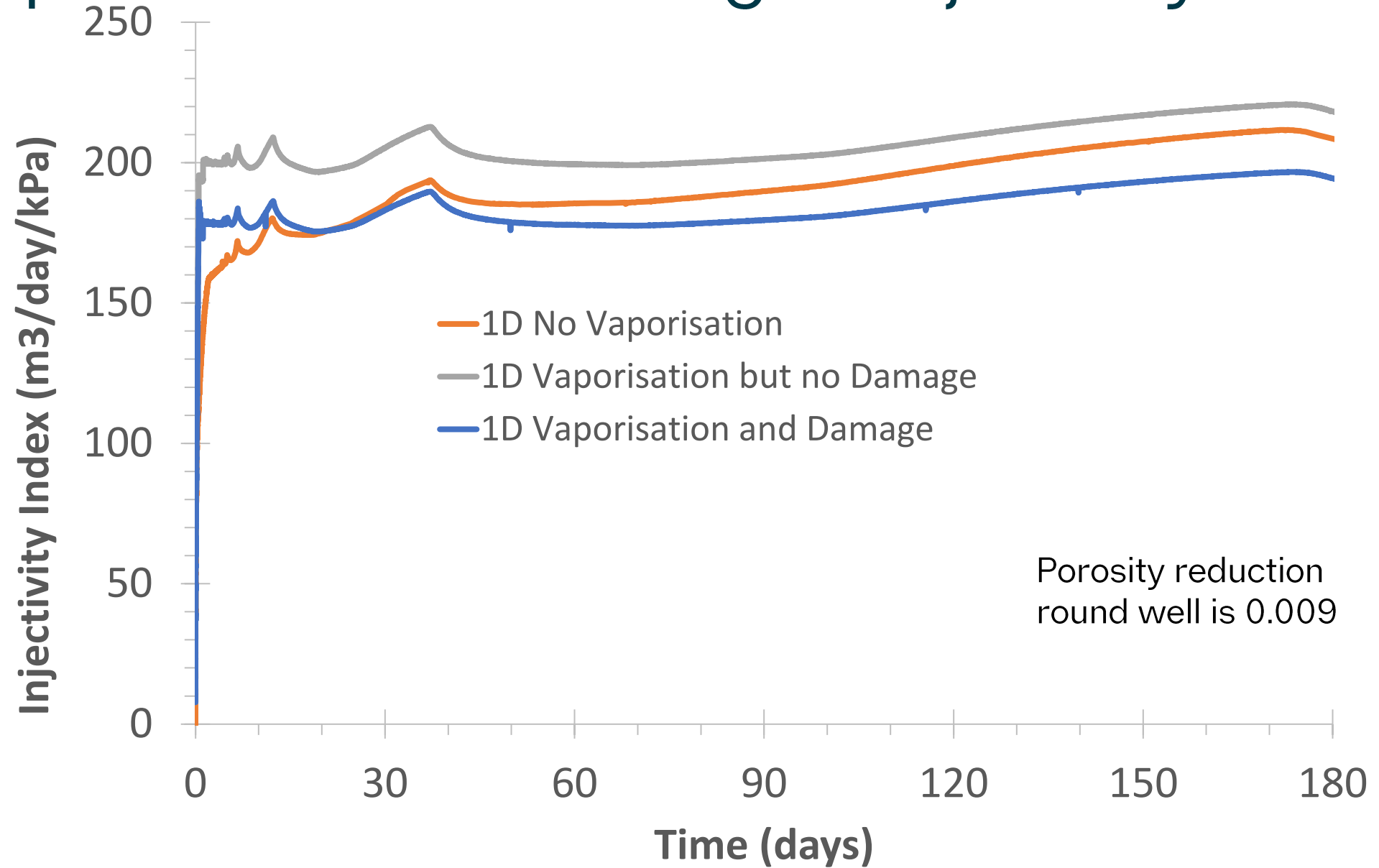
1D Vaporisation but no Damage – Mobilities



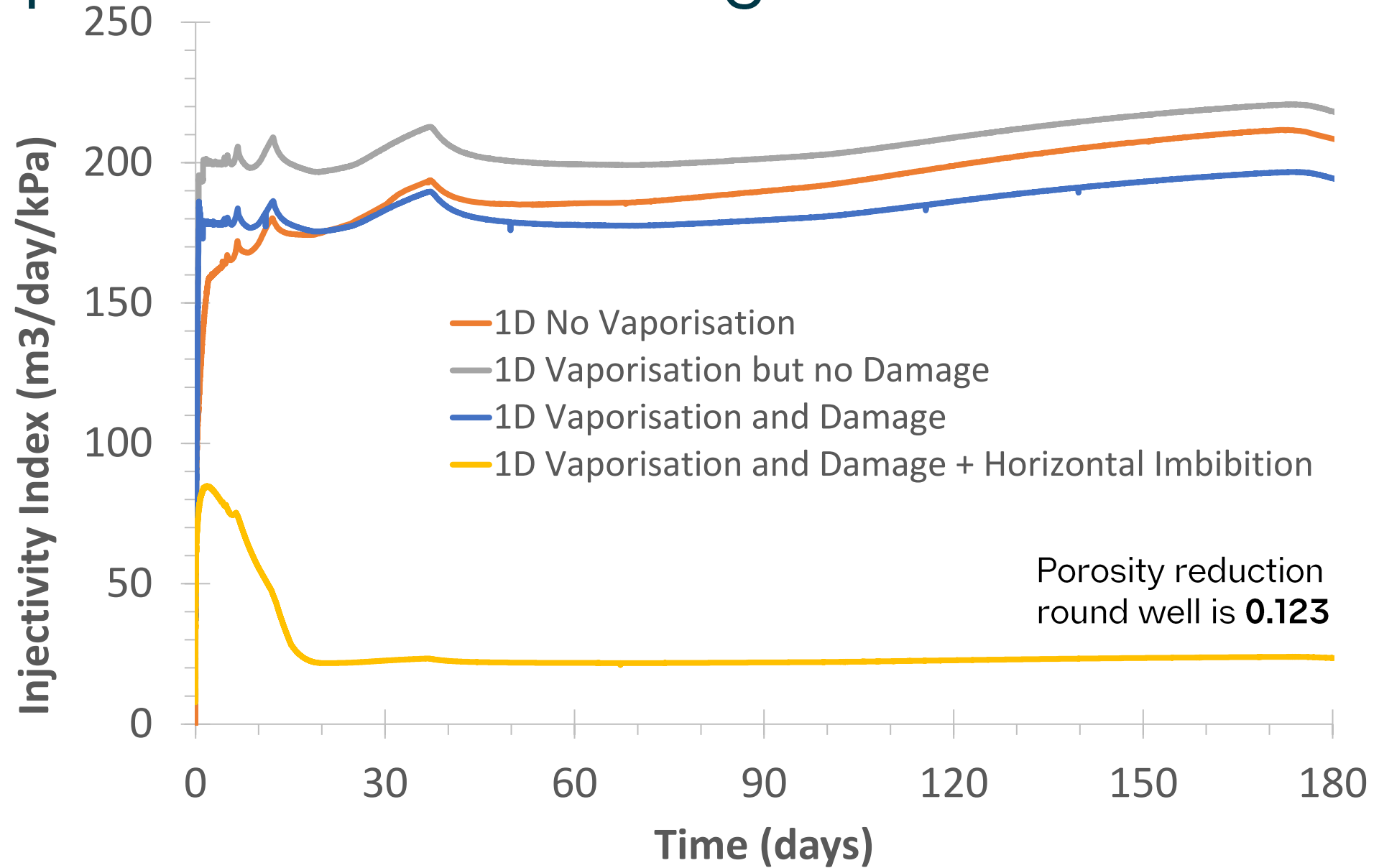
1D Vaporisation but no Damage – Injectivity Index



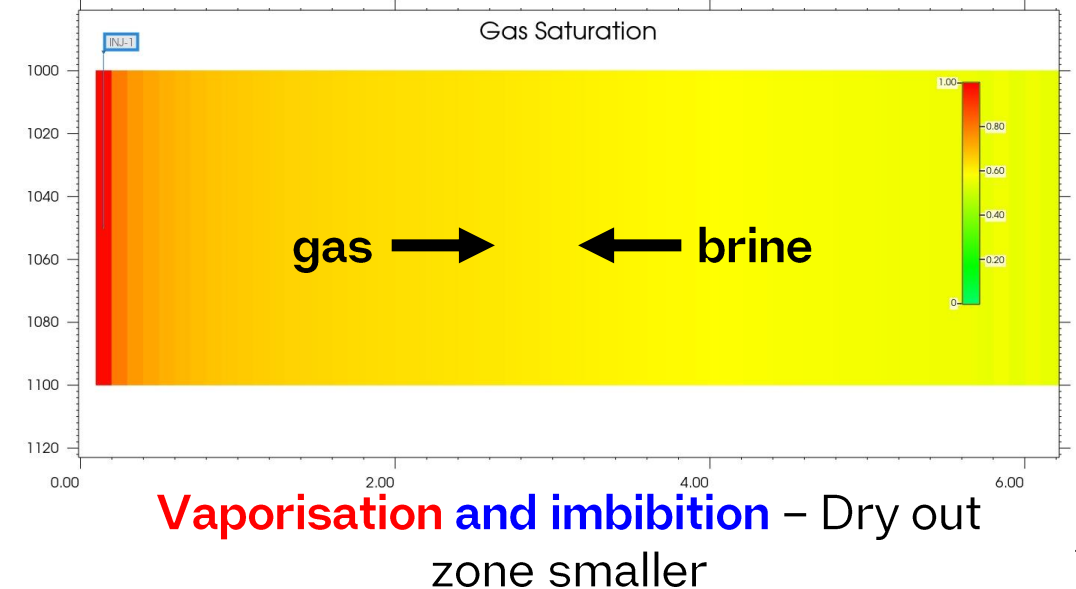
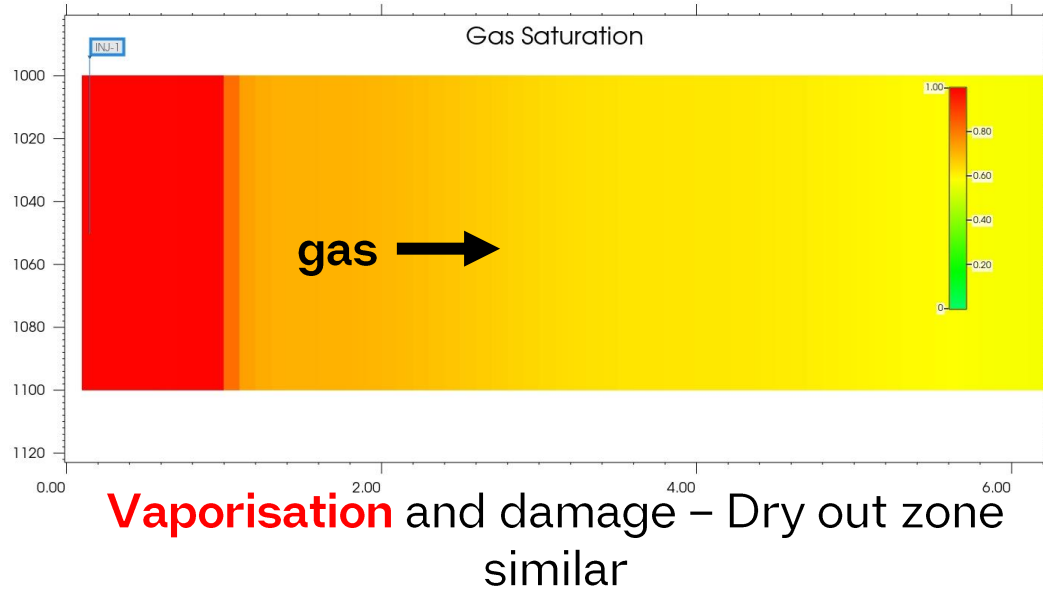
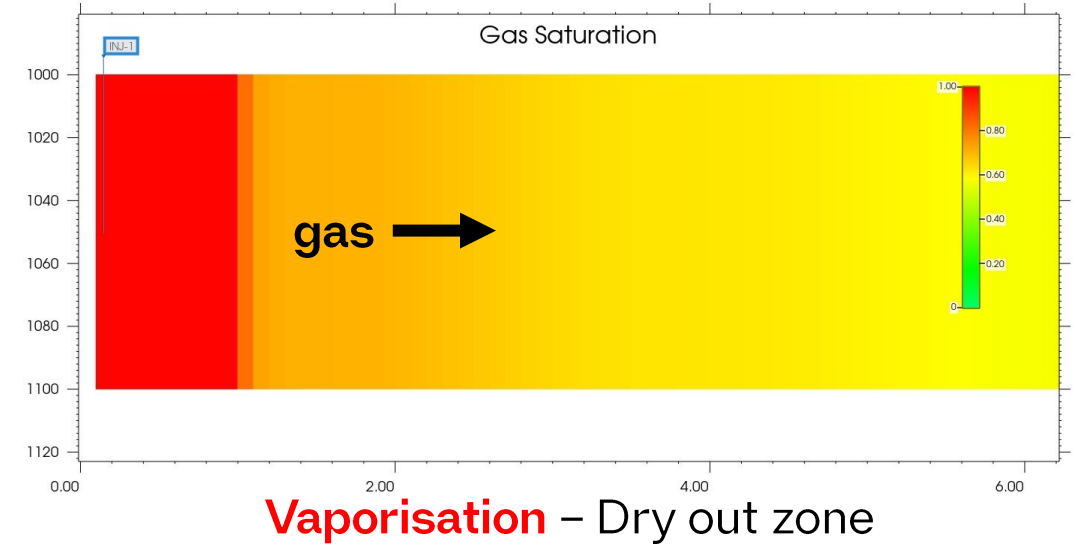
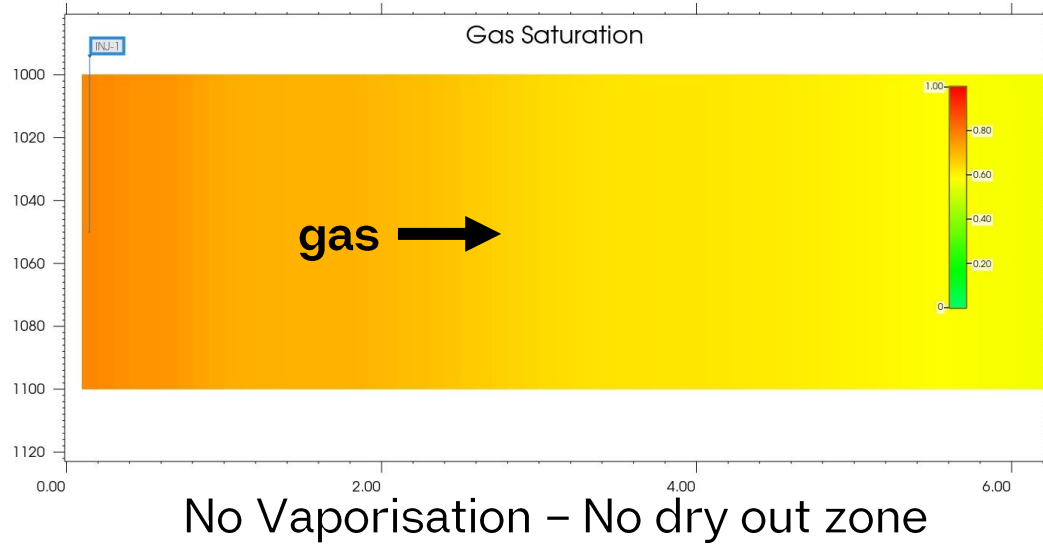
1D Vaporisation and Damage – Injectivity Index



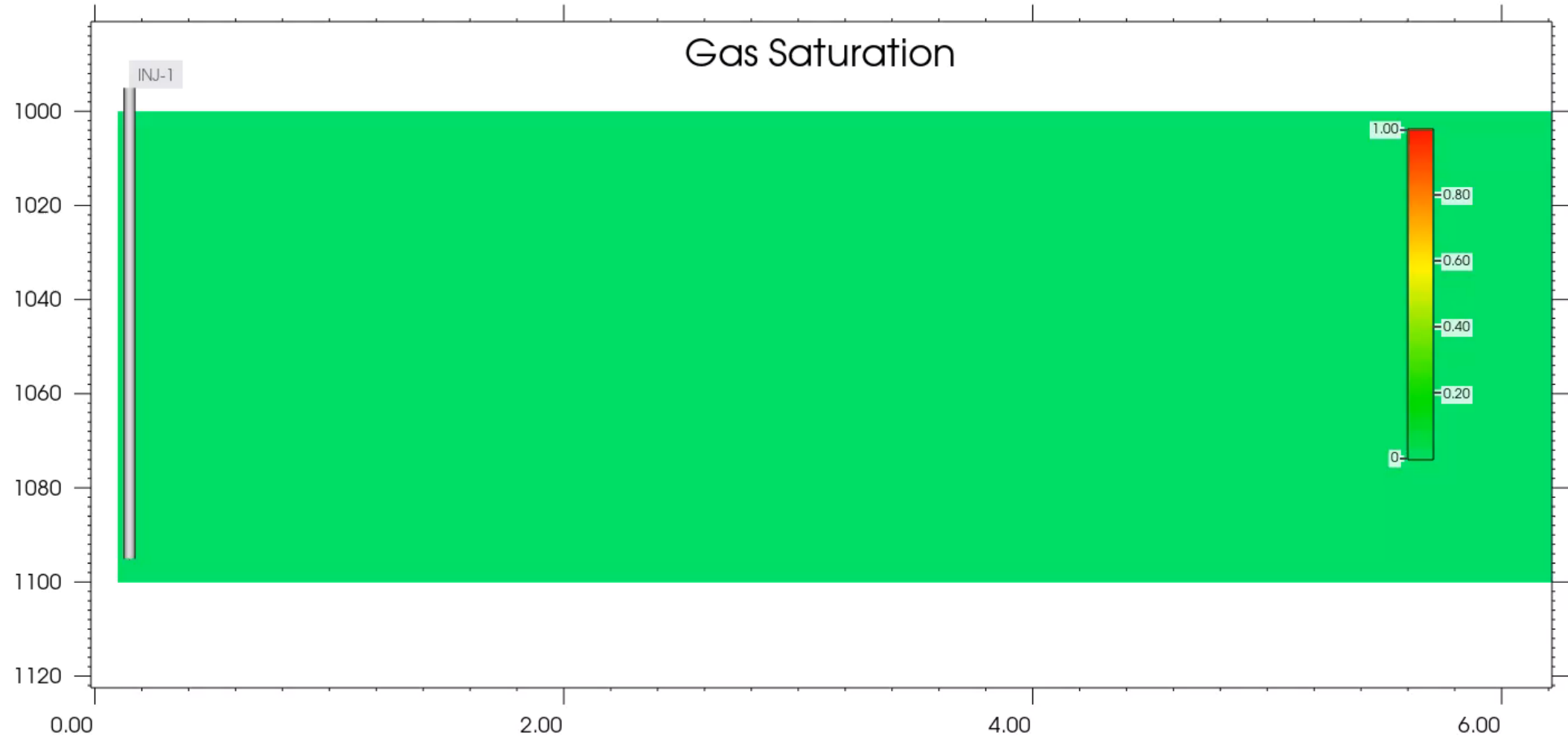
1D Vaporisation and Damage with Imbibition



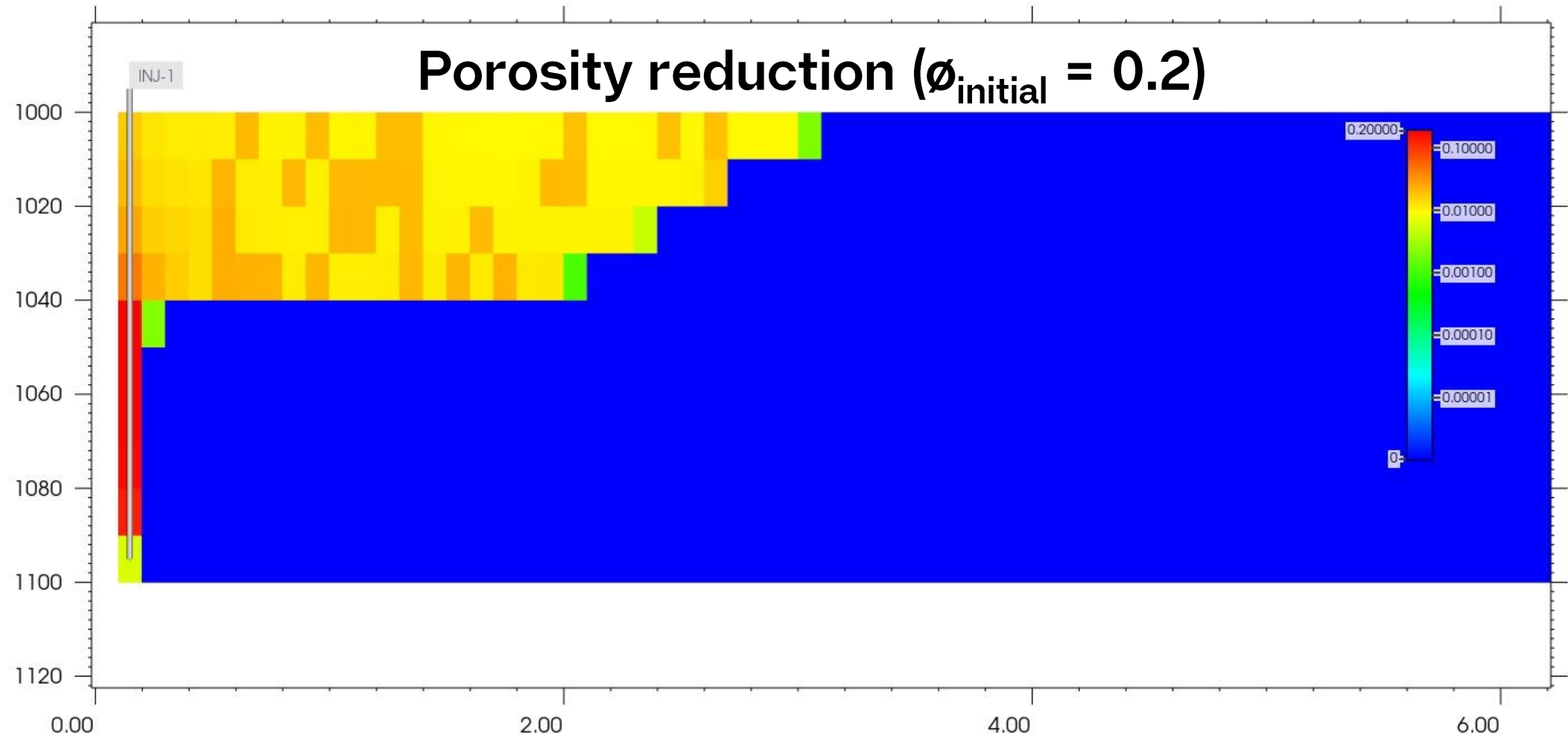
Size of Dry Out Zone



2D Vaporisation and Damage with Imbibition



2D Porosity Change



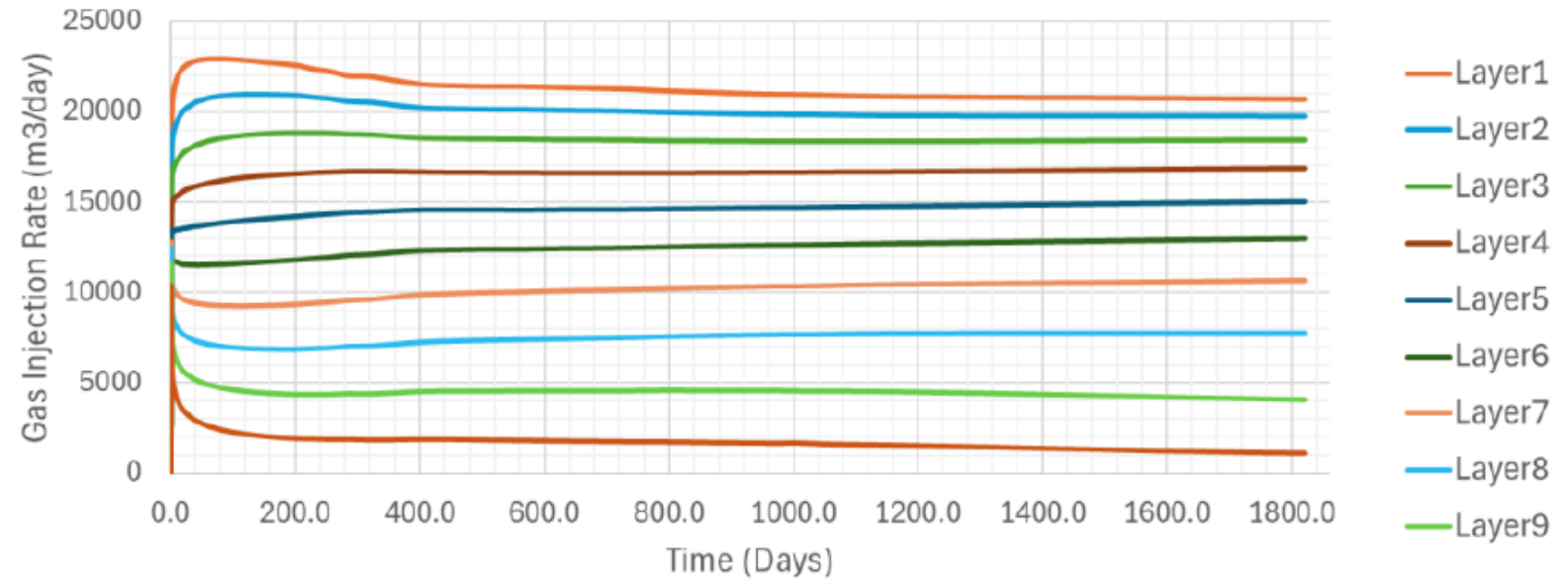
Effect of Gravity

- Density difference between CO₂ and water
- Higher mobility of CO₂ than water
- Effect of imbibition

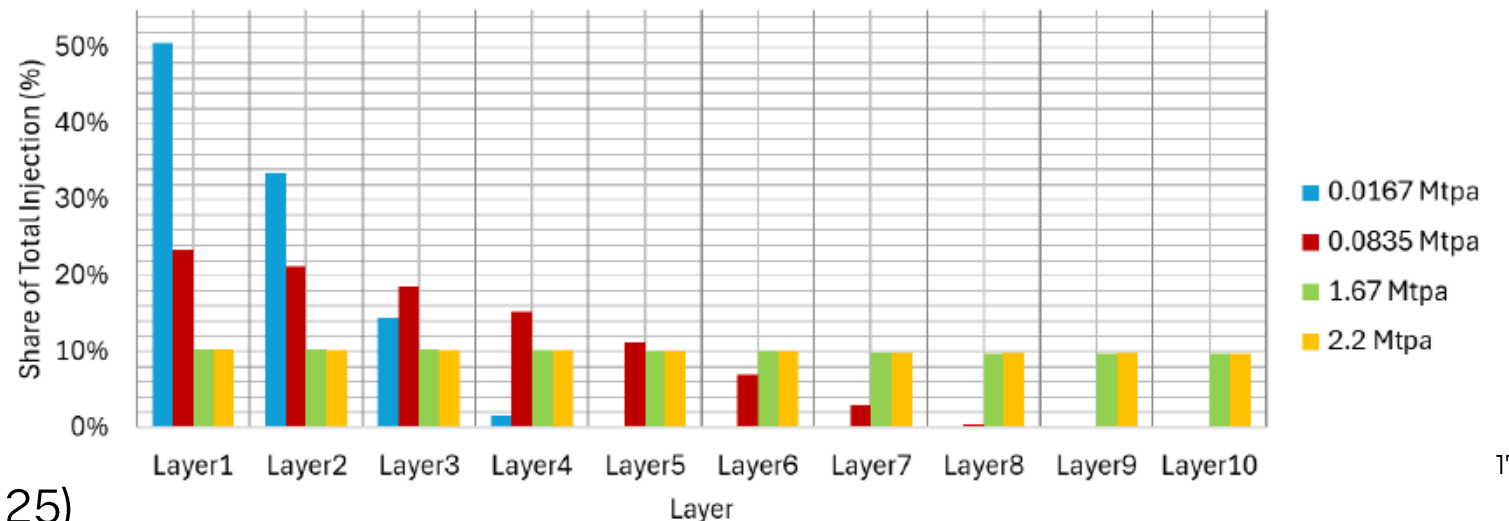
..... all promote gas injection at top of well, and brine recharge and halite deposition towards bottom of well

Q_{inj} = 0.167 Mtpa over 100m interval

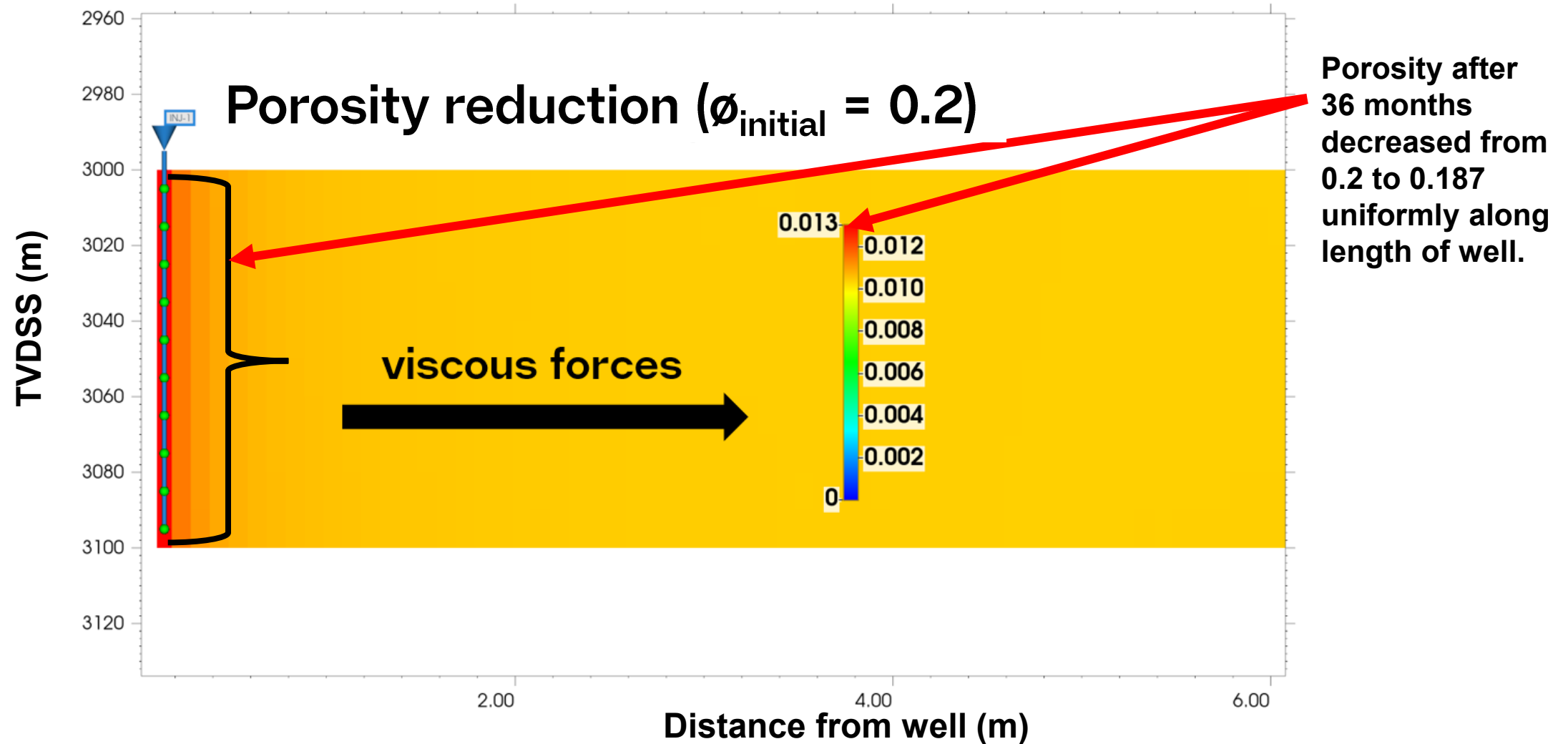
Gas Injection Rate Per Layer Vs Time



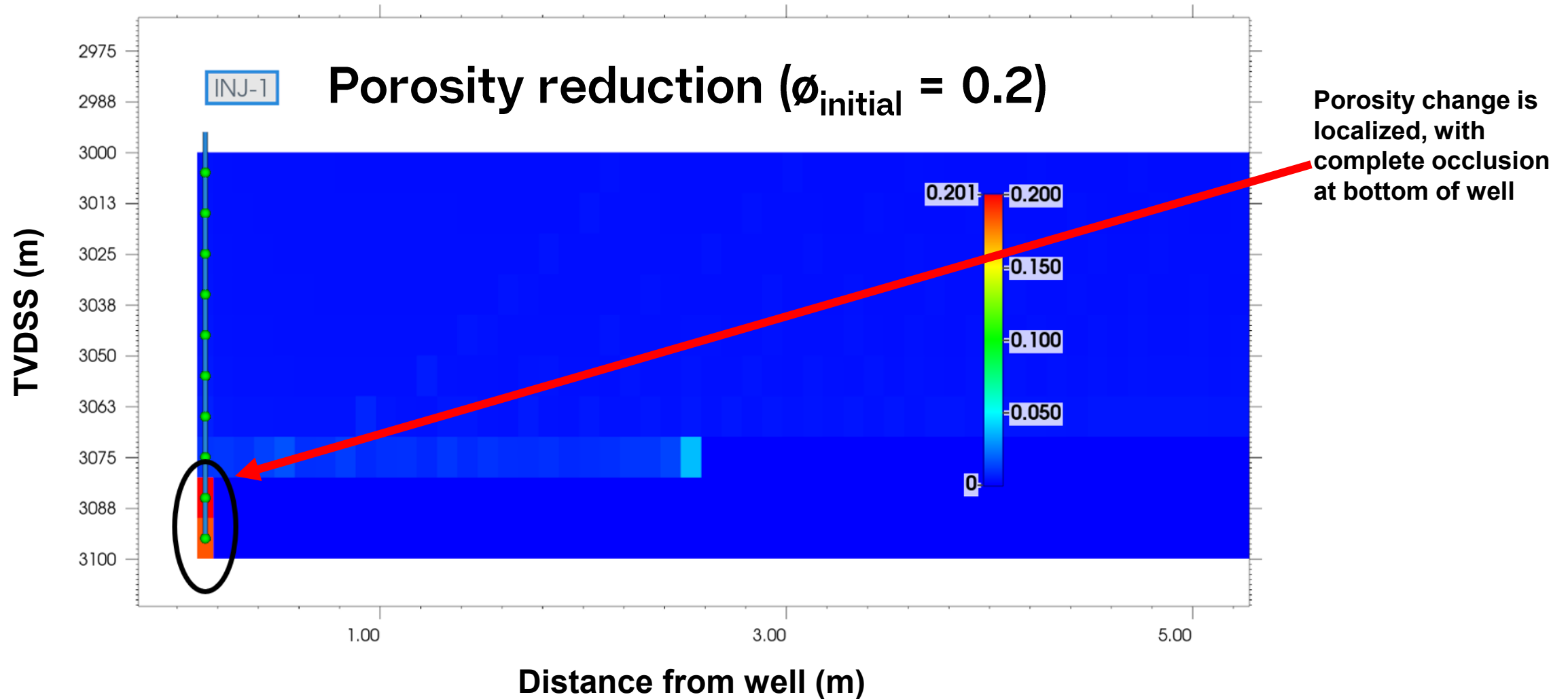
CO₂ Injection Distribution by Rate



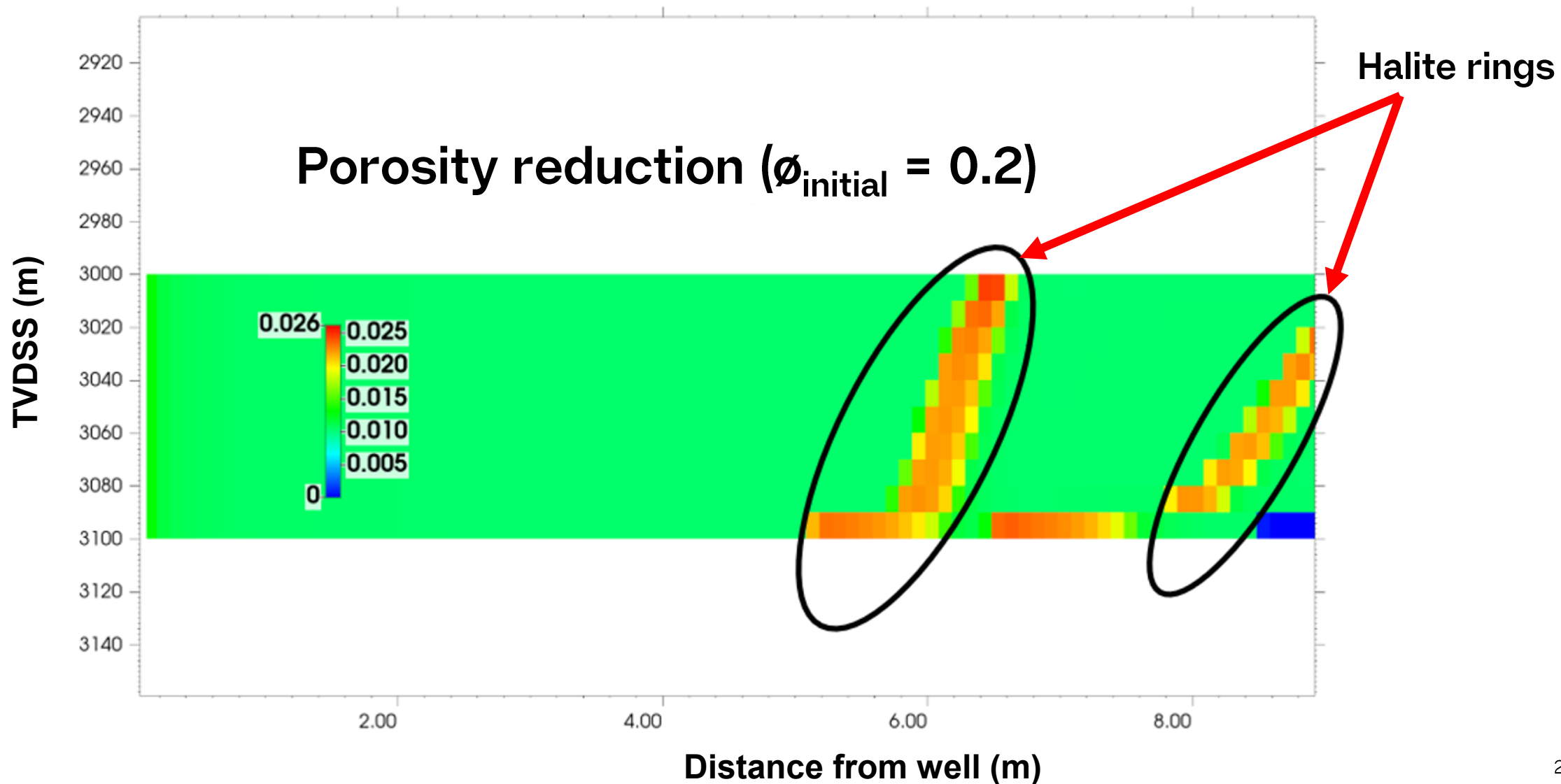
1 Mtpa Injection Rate – Negligible Porosity Loss



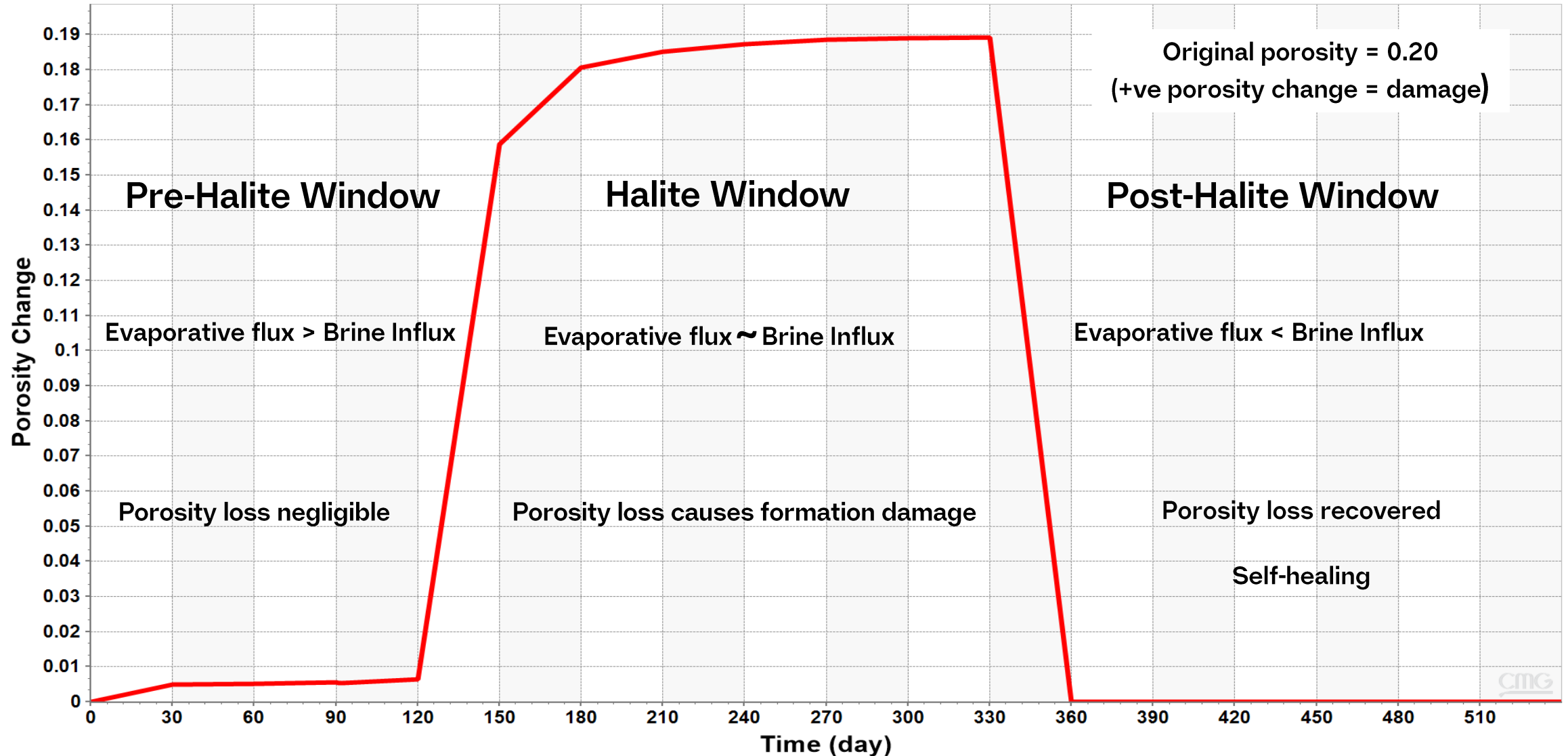
0.05 Mtpa Injection Rate – Damage at Well Bottom



Intermittent Injection Rate – Minor Loss in Rings



Washwater Treatments – Halite Window



Washwater Challenges

- Water-only wash treatments may lead to
 - corrosion risk (CO_2 plus water = carbonic acid)
 - hydrate risk
- Recommendation to include in wash water treatments:
 - thermodynamic hydrate inhibitor such as Mono Ethylene Glycol (MEG) plus water as a “water wash” mixture, or
 - kinetic hydrate inhibitor (KHI) and/or
 - corrosion inhibitors

Conclusions

- **Evaporation** only occurs into **dry CO₂** stream
 - evaporation of water alone **increases** injectivity
- Salt deposits occur when
 - dissolved salts are present in formation brine
 - brine can flow into dry out zone due to capillary and gravity effects
- **Greatest damage** to CO₂ injectivity occurs when
 - **brine salinity is higher** (but can occur at any salinity)
 - **brine flux** into dry out zone is **close** to **but less than evaporative flux**
- **Damage minimised when injection rates are high**
 - better to have intermittent high rate than continuous low rate injection
- **Wash water treatments** beneficial in early periods
 - but need to **manage corrosion** and **hydrate risks** using additives

Acknowledgments

- Sponsors of **FAST JIP** at Heriot-Watt University

Baker Hughes 

 **CHEMISERVIS**

CLARIANT 



equinor 

HALLIBURTON

 **Harbour Energy**



Y-TEC

- **CMG Ltd** for use of **GEM** reactive transport reservoir simulator



- **Energi Simulation** for funding the chair in *CCUS and Reactive Flow Simulation* at Heriot-Watt University



'a foundation for the future'

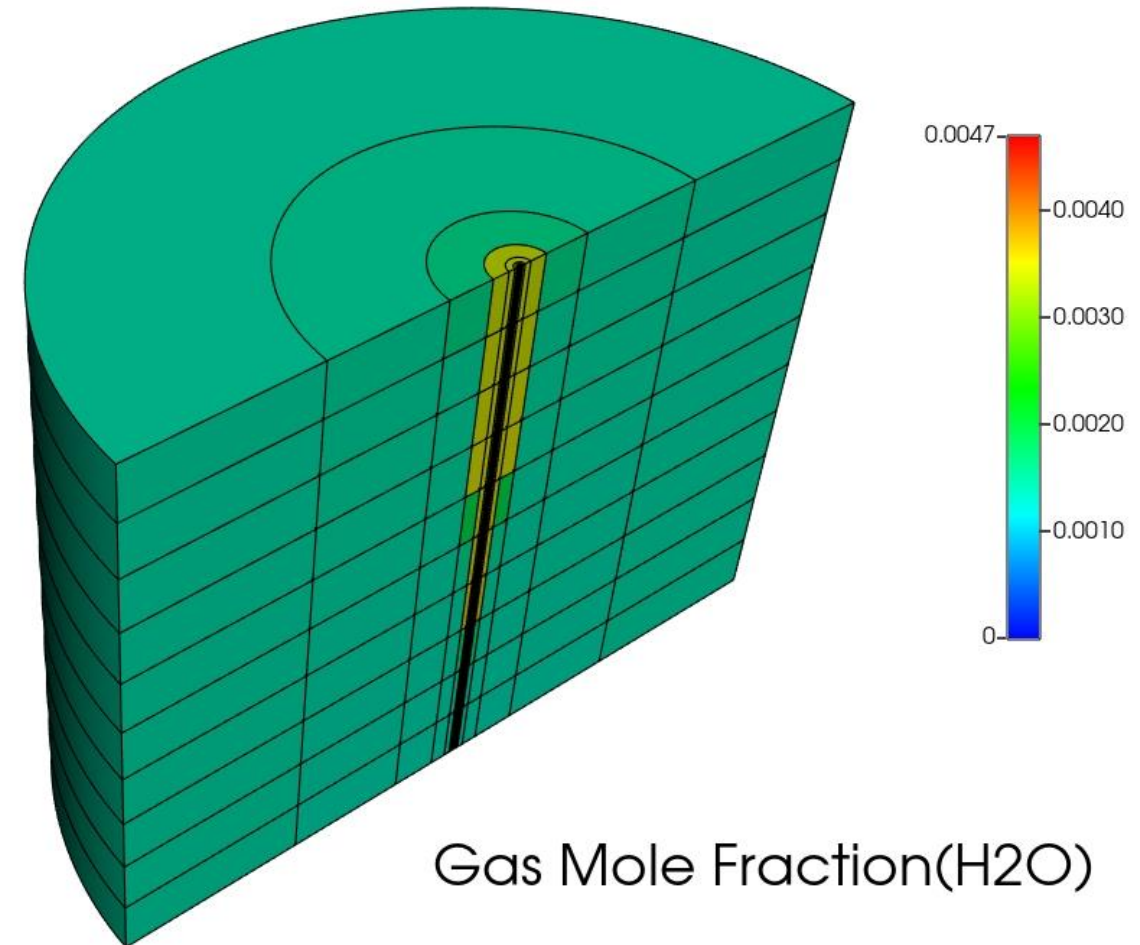
- **PTDF** for funding scholarship held by Oluwatosin Ogundipe



PTDF

Model Setup

PROPERTY	VALUE
Geometry	1D Radial (110 x 1 x 1 cells)
Dimensions	2 km x 180° x 100 m
Radial cells	100 x 0.1 m, then increasing exponentially to outer cell of 1 km
Porosity	0.2
Outer cell pore volume multiplier	1x10 ⁵ (constant pressure boundary)
Rock compressibility	1x10 ⁻⁶ 1/kPa at 10,000 kPa
Permeability	100 mD
Depth	1 km
Initial pressure at 1 km	10,000 kPa
(Isothermal) temperature	50 °C
Water compressibility	4.5x10 ⁻⁷ 1/kPa at 10,000 kPa
Water viscosity	0.39 cP
Initial water saturation	1
Aqueous components	Na ⁺ , Cl ⁻ , CO ₂ (Henry's Law)
Activity model	Pitzer
Formation brine composition	5.6 M NaCl
Gas phase components	CO ₂ , CH ₄ , H ₂ O
Equation of State	Peng Robinson
Injected gas	pure CO ₂
Well type	Vertical (100 m)
Injection rate	76,200 sm ³ /day (=0.1 MT/yr)
Injection period	6 months
Permeability reduction model	Kozeny-Carman (exponent 2.0)



What is Effect of Imbibition?

- Brine continuously re-invades dry out zone due to capillary pressure
- As brine evaporates
 - Halite deposits
 - More brine is imbibed
 - Deposition greatest where rate of evaporation and rate of imbibition are matched
- What about gravity?

