

# **NOV Process Partner**Conversion of Production Separator to Induced Gas Flotation Unit

Understand-Define-Validate-Deliver-Support

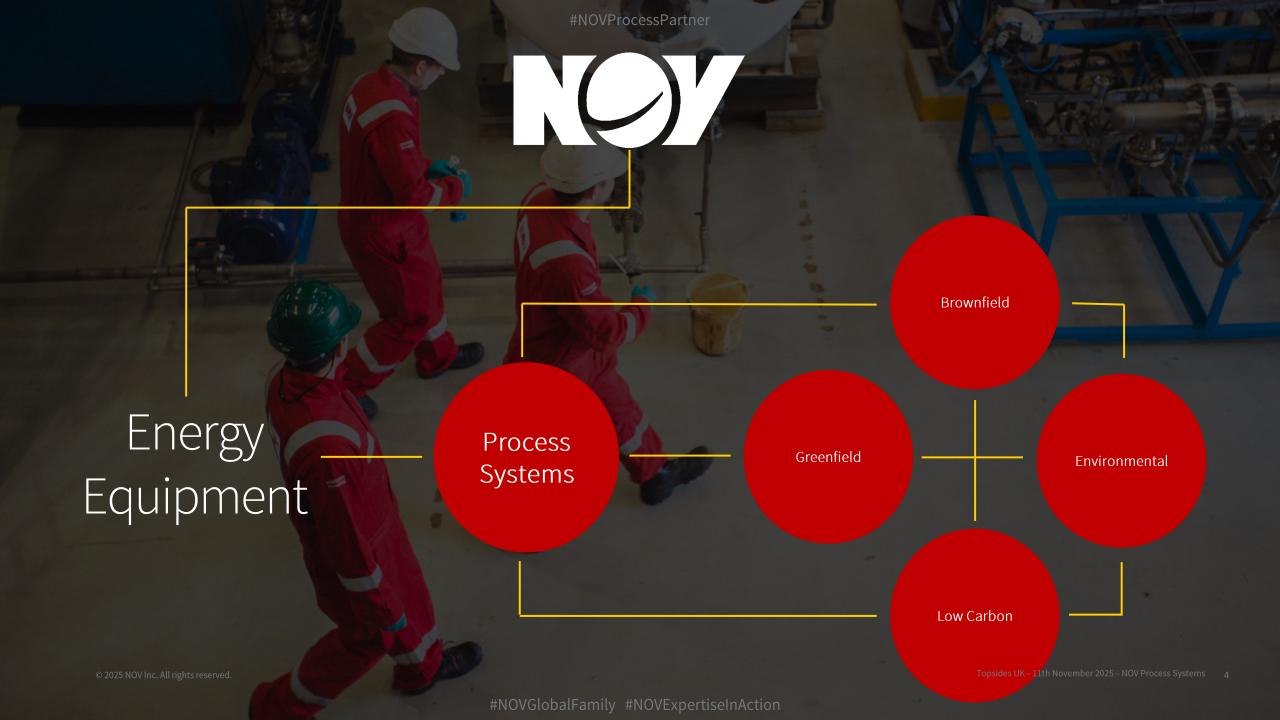
David King (Business Development & Sales Manager) – NOV (Presenting)

James Vanjo-Carnell (PW Product Line Manager) – NOV

Neil Gourlay (OPUS Team Process Manager) – NOV







## **Process Systems**

Your value creation energy partner











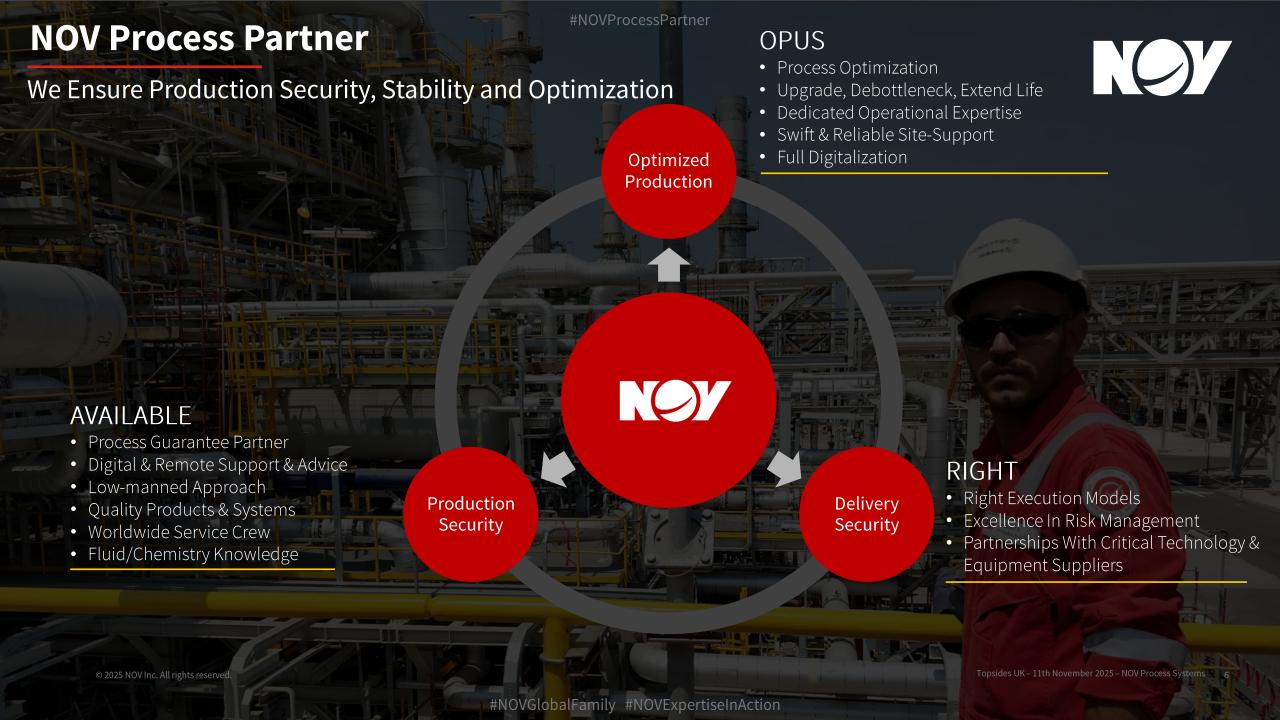












## **Process Systems**

#### The OPUS Approach



#### **Customer Pain Points**

Capacity | Performance | Reliability

#### Understand

Data collection | Site Assessment | Fluids Characterization

#### Phase 1 - Understand

- Identify root cause of challenges
- Detailed analysis of the existing process
- · Site assessment if needed to gather data
- · Careful assessment of fluids chemistry

#### Phase 4 - Sustain

- · Operations and maintenance support
- Spare parts management
- Digitalization/remote support services
- · Process studies for increased production

## Phase 3 – Deliver and Optimize In order of priority:

- Optimize the existing process
- · Upgrade existing process equipment
- · Design and install new package
  - Install, start-up and optimize
  - Guaranteed on-spec performance



## **Deliver / Optimize**Optimization | Retrofit | Package Supply | Lifecycle Services

#### **Define / Verify** Study | Modelling | Design

#### Phase 2 - Define and Verify

- Specialist process and detailed engineering
- Performance models built on 30 years of process verification & optimization
- · Physical modelling
- · Computational fluid dynamics (CFD)
- Finite element analysis











#### The Motivation

LP Separator

Train 1&2

Recovered Oil Tank

Where does it all begin...

Gas Processing

Crude Degasser

PDT



#### **Objectives:**

16" Hydrocyclone

24" Hydrocyclone

LP Separator Hydrocyclone Skid (two trains)

- Debottleneck Capacity Target 75kbwpd
- Reduce Oil-in Water Content Target <29ppm avg.

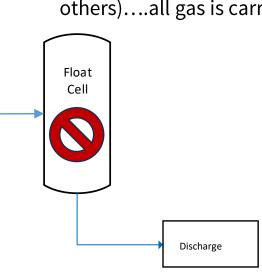
Water Clarifier

Injection

- Reduce gas in PW Avoid carry-under
- Minimal CAPEX Solution

#### **Original PWT System:**

- Vertical hybrid CFU type flotation unit.
- Flotation cell contained a severe design flaw – not fit for purpose.
- No operational performance rental treatment used instead (high OPEX).
- Root cause confirmed via CFD and Nucleonic tracer survey (by others)....all gas is carried under!



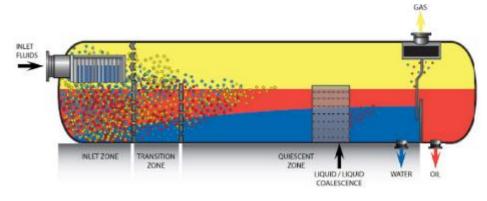
Water Stream Gas Stream

Oil/Reject Stream

## The Challenge

What did we do...

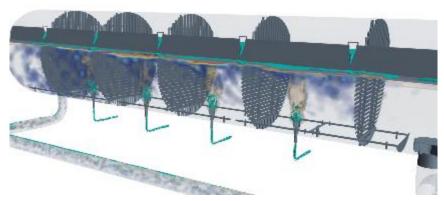






#### **Donor Vessel Requirements:**

- Horizontal or vertical vessels considered.
- Suitable number of nozzles needed; advantageous placement helpful but not essential.
- Suitable number of internal clips needed no welding no bonding allowed.
- Adequately sized to get meaningful performance, but did not have to be limited to 'Standard Norms'.

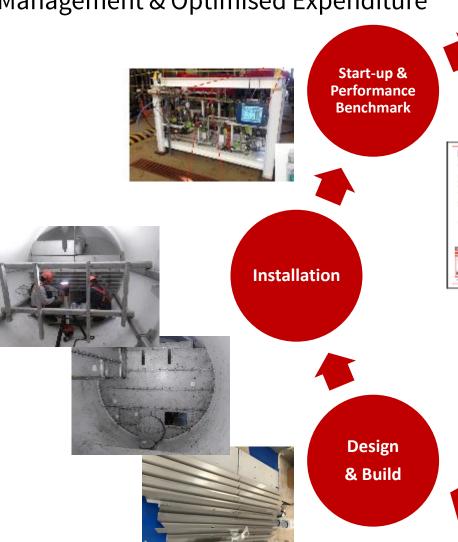


#### **Selected Candidate:**

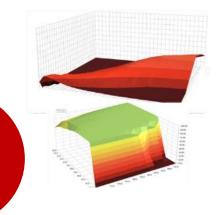
- Horizontal IP Separator.
- Several drain nozzles intended for sand handling system present → flotation gas bubble inlets.
- Feed/outlets & instrumentation nozzles also well placed.
- Several baffles already in the vessel → clips!
- Well (but aggressively) sized.
- Moderately helpful location on the facility.

## **The Approach – OPUS**

Risk Management & Optimised Expenditure

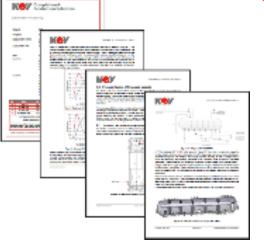


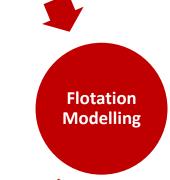




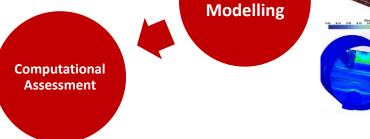


Note: some details deliberately obscured to protect NOV IP.

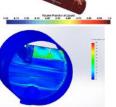








**Physical** 

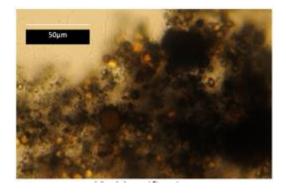


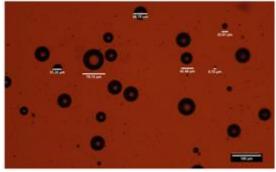
### **The Site Survey**

#### **Building Understanding**









## **At NOV Orkney Water Test Centre:**

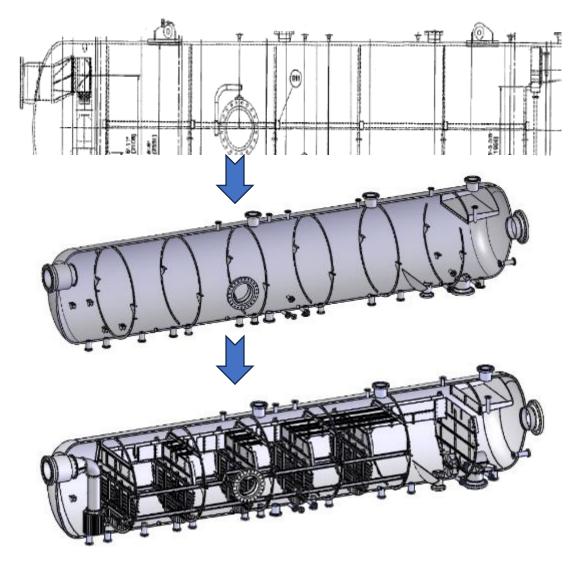
- Client water and oil.
- Fluid microscopy.
- Technology compatibility (Mare's Tail precoalescer).

#### At Site:

- Droplet sizing.
- Performance Analysis (site test of DOHC and Mare's Tail pre-coalescer).

### The Desktop Study

#### **Understanding Options & Defining Solutions**





### **Repurposing of equipment:**

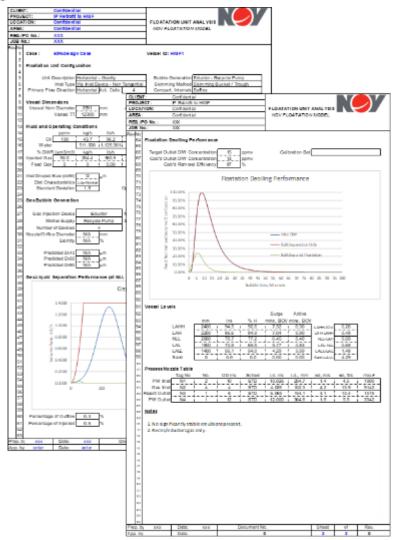
- Multiple vessels considered as donor vessel unused production separator selected (2.5m ID x 12m TT).
- Repurposing existing float unit microbubble pumps also considered - not viable, ejector technology preferred.

## **Uncertainty:**

- Best available vessel did not have as much. residence time as typical for HIGFs – flotation model used to quantify short fall.
- Scaled physical testing (580mm ID) of final solution considered as a risk mitigation step.

#### The Flotation Modelling Tool

#### Validating the Solution





#### The Model:

- Semi-empirical universal model based on various separation and flotation correlations, benchmarked against Flotta and Field data.
- Jointly created by NOV and a SuperMajor to offer technology independent hydraulic and performance analysis of flotation units

### The Output:

- Determine impact of smaller-than-typical vessel size.
- Confirm gas bubble and oil removal performance.
- Estimate performance with and without deoiler chemistry.
- Confirm impact of droplet size, flow rate, gas rate.

## The Physical Modelling Set-up

#### Validating the Solution in the Test Hall





5ppm Deoiler Chemical

10ppm Deoiler Chemical

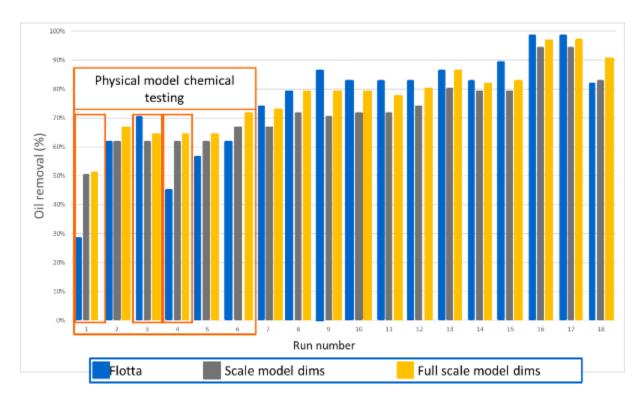




20ppm Deoiler Chemical

100ppm Deoiler Chemical

Visual testing demonstrating deoiler overdosing



#### **Test Conditions:**

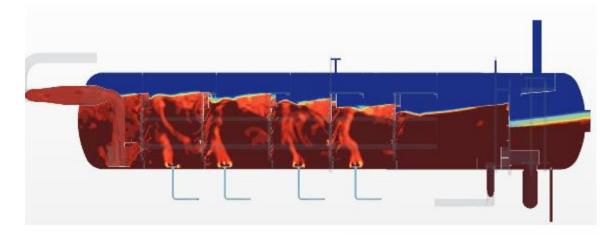
Client crude + seawater. 100-300mg/l inlet OiW. 7-24um dv50 droplet size

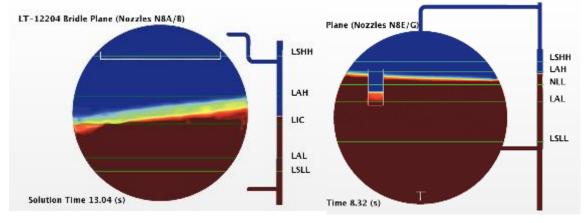
W/wo chemicals. Low/med/high gas rates. Low/med/high flow rates.

## The Computational Modelling Set-up

#### Validating the Solution with CFD







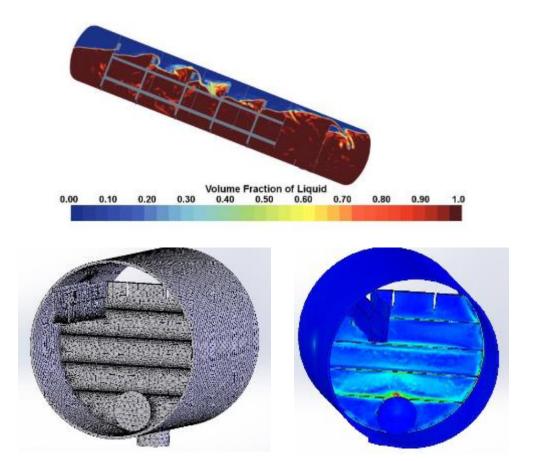
#### **CFD**

- Verify liquid behaviour during rough sea states (facility motion, operating and survival cases).
- Verify level instrument response vs actual liquid behaviour (bridles used).
- Check skimming behaviour and oily water compartment sizing.
- Generate force loading data for FEA (survival condition).

## The Computational Modelling Set-up

#### Validating the Solution with FEA





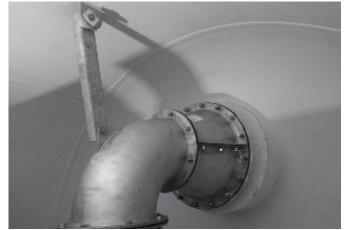
#### **FEA**

- Confirm existing vessel clips can withstand loading during survival conditions.
- Maximum corrosion allowance applied to clips.
- Force loads from CFD (extreme survival case) applied into the FEA model. A 'force monitor' was applied in the CFD model to record the expected force loading at important points over the course of multiple motion cycles.
- Attention paid to verify no resonance behaviour is occurring.

#### **The Solution Delivered**

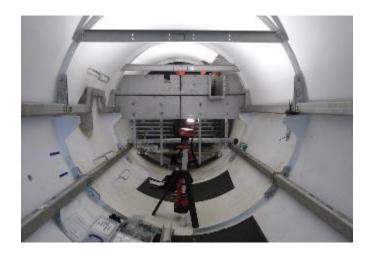
#### Designed – Built - Installed















Vessel retrofit timeframe: 2 weeks
Topsides UK- 11th November 2025 - NOV Process Systems 17

#### **Performance Assured**



Start-up & Performance Benchmarking

Data Redacted

Very fine margins.... to prevent erroneous / overly optimistic outputs the float Model is normally 'capped' at <5mg/l or <15mg/l depending on the application .....very difficult to predict reliably below this value!

#### **Performance Assured**



Start-up & Performance Benchmarking

**Data Redacted** 

Data with 5mg/l cap applied suggests that it is a good 'bottom end' for the model (in this case), overall efficiencies line up well..

#### **Conclusions**

#### Collaborative Approach – Proprietary Technology – Assured Performance



#### Collaborative Approach:

- Several years of diligent validation design work has led to a robust retrofit design.
- Cross-party planning of the retrofit and subsequent startup scope minimised interfacing issues
- Versatile & experienced team efficiently dealt with execution challenges.

#### Proprietary Technology:

- NOV's Flotation Model provided clarity on the initial direction taken, no possible solution using standard design rules.
- Test Hall modelling and CFD to validate flow dynamics in extreme cases.
- Complete supply of retrofittable NOV IGF hardware.

#### Assured Performance

- Validation of Process & Mechanical design throughout in recognition of complexity of the work.
- Site-based install, commissioning and early operational support.
- Benchmarking and backchecking performance against model and physical test data offered confidence and a good basis for operation going forward.

#### **NOV as Integrated Process Partner for Life of Operation**

## **NOV Process Partner**

Conversion of Production Separator to Induced Gas Flotation Unit

Understand-Define-Validate-Deliver-Support

**Questions?** 

David.King3@nov.com

November 11, 2025



