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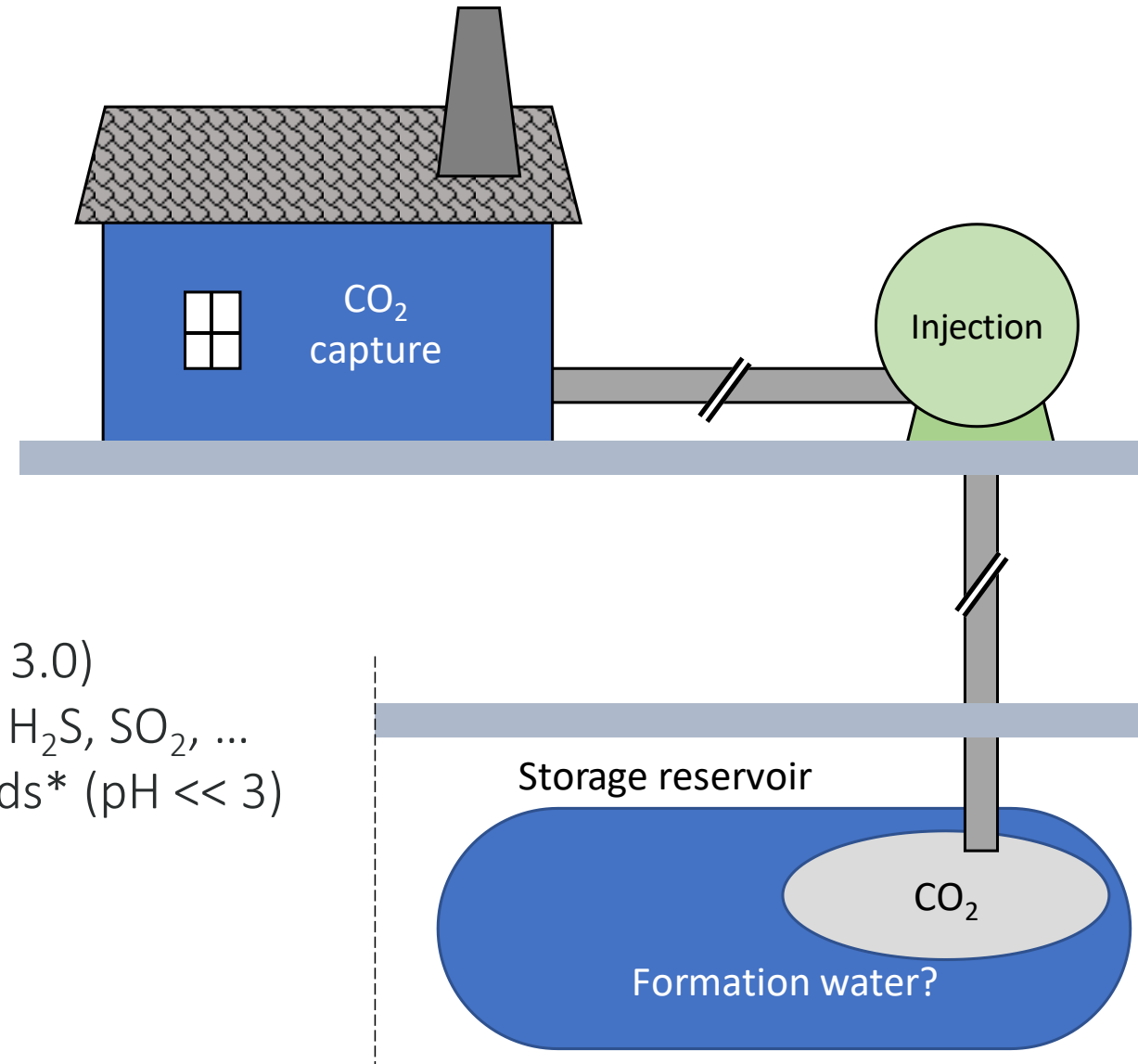
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# Well material selection for CO<sub>2</sub> storage

Gaute Svenningsen  
Institute for Energy Technology (IFE)  
NO-2027 Kjeller  
Norway

# Introduction

- Oil and gas wells have always been exposed to CO<sub>2</sub>, but at “moderate” levels, e.g. ~ 0.1 – 10 bar CO<sub>2</sub>.
- The general design codes still apply to CO<sub>2</sub> injection wells, but...
- Injection wells may have >> 150 bar CO<sub>2</sub>
  - Low pH, particularly in condensed water (< 3.0)
  - Constant supply of impurities like O<sub>2</sub>, NO<sub>2</sub>, H<sub>2</sub>S, SO<sub>2</sub>, ...
  - Impurities may react and create strong acids\* (pH << 3)
- Long-life of injection well perspective
- No leak after injection has stopped.



\* Morland, Tjelta, Norby, Svenningsen, International Journal of Greenhouse Gas Control, 87, (2019) pp. 246-255.



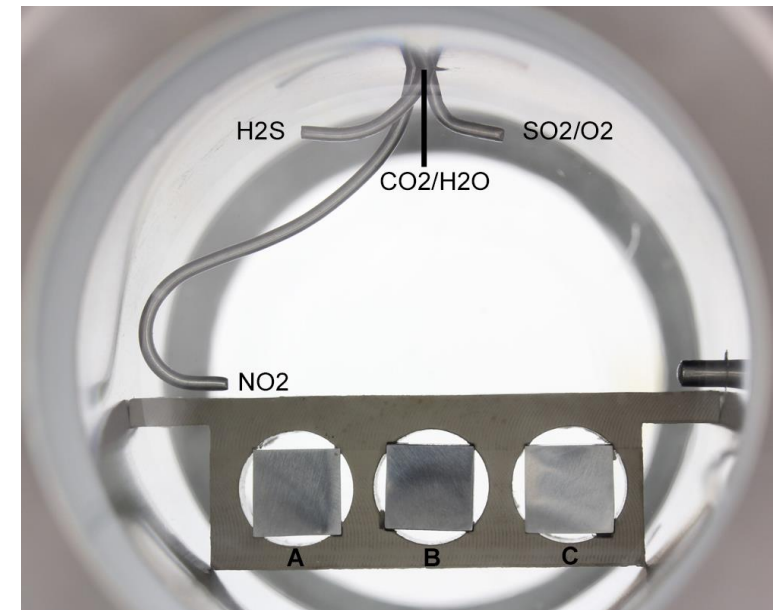
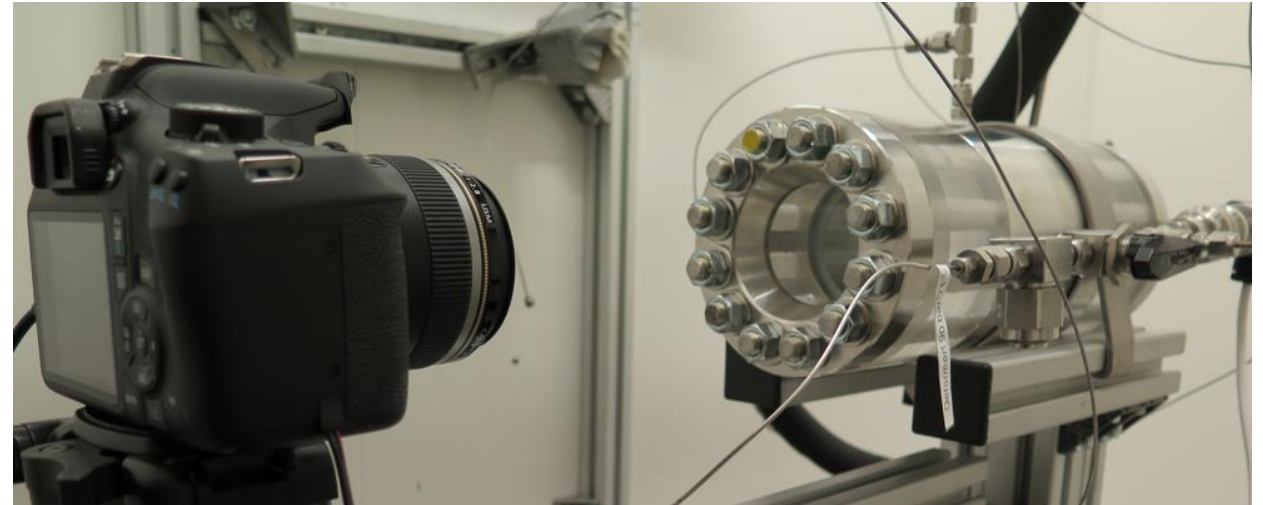
# Verifying the material performance in the lab

Use realistic test conditions (along the CCS chain)

- **A: CO<sub>2</sub> transport in pipelines**
  - Low to intermediate temperature (0 – 50°C)
  - High pressure >70 bar
  - No water: Carbon steel can be used
- **B: CO<sub>2</sub> transport with ships**
  - Low temperature (-40 - +10°C, low pressure)
  - No water: Carbon steel can be used
- **C: Well / down hole (CO<sub>2</sub> injection)**
  - High pressure and temperature
  - Water is present (formation water or condensed water)
  - Use CRA (Corr. rate of carbon steel >> 10mm/y)

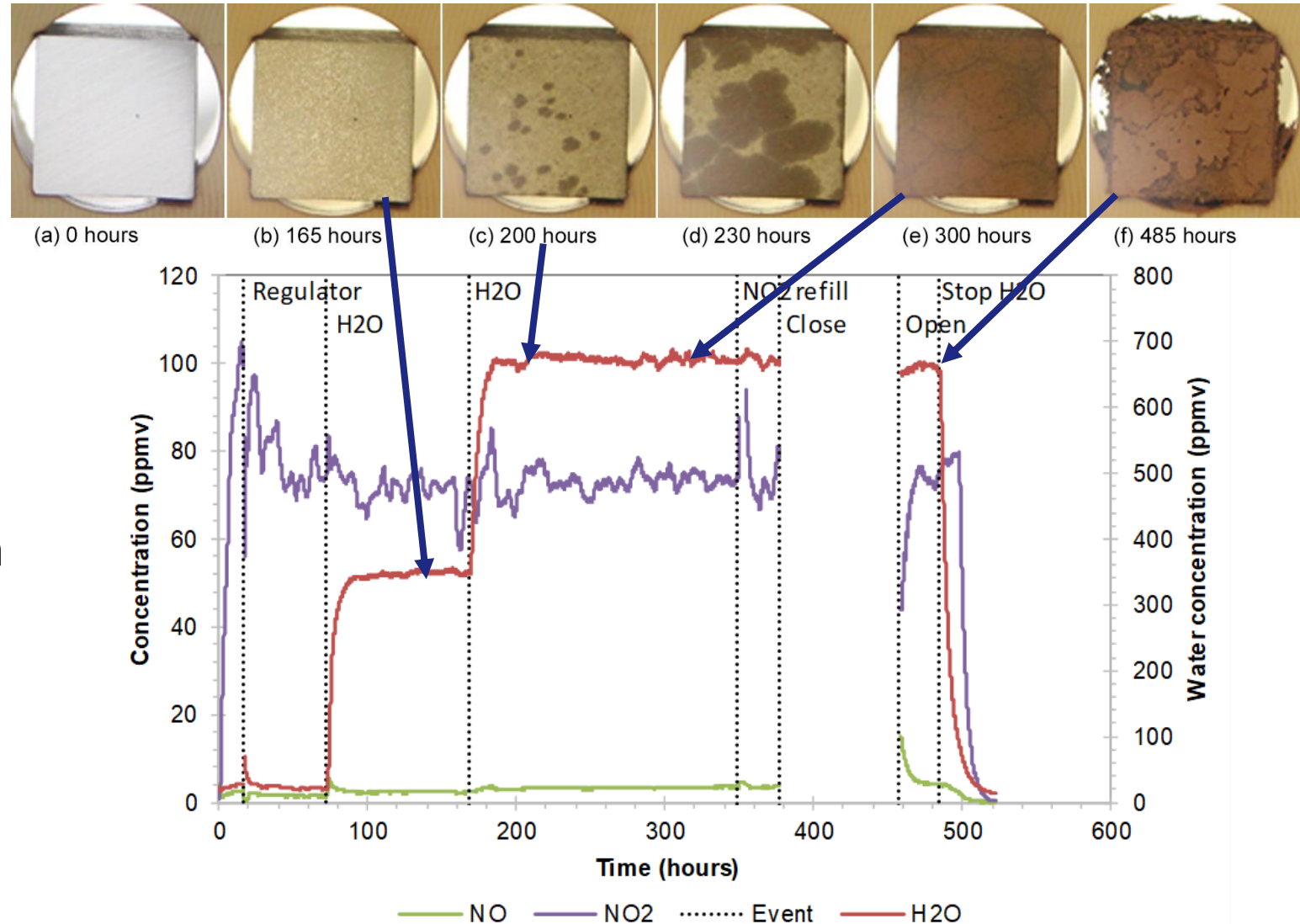
Impurities must be included in the testing

- Origin from flue gases and capturing processes
- Continuous feed
- Low concentration, typically 10 – 100 ppm-mol level



# CO<sub>2</sub> pipeline test: CO<sub>2</sub> with NO<sub>2</sub> and H<sub>2</sub>O\*

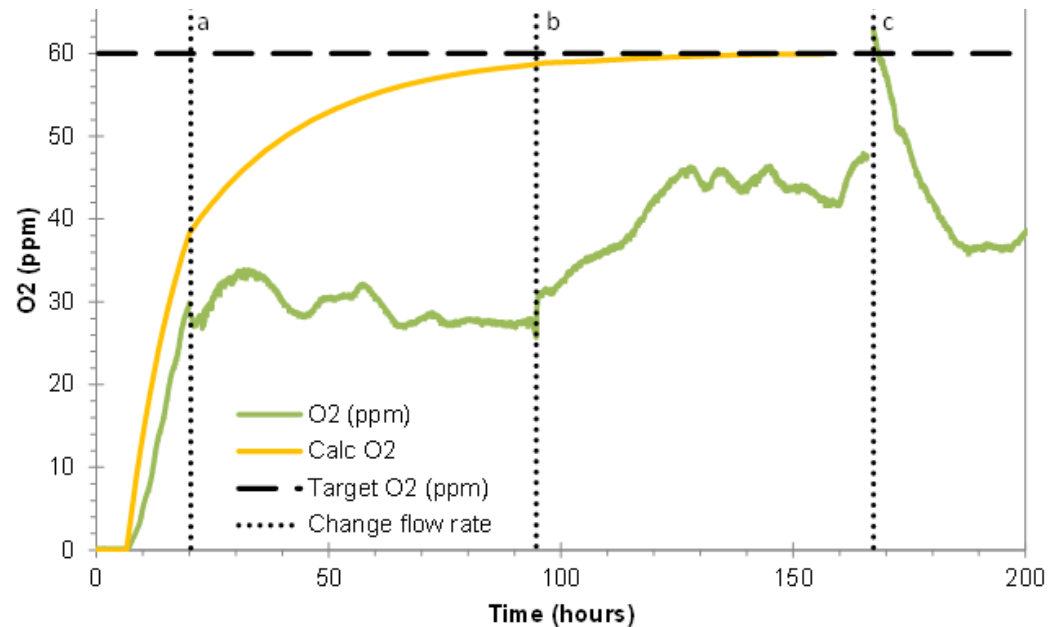
- Carbon steel
- Dense phase CO<sub>2</sub>
- 100 bar / 25°C
- 72 ppm-mol NO<sub>2</sub>
- Stepwise increase of H<sub>2</sub>O:  
24 => 350 => 675 ppm-mol  
(the water was fully dissolved in the CO<sub>2</sub> bulk phase, no liquid water present)



\*Morland, Norby, Tjelta, Svenningsen, *CORROSION*, 75, 11 (2019) pp. 1327-1338.

# Down hole test: SCC test of 13Cr with O<sub>2</sub>\*

- 13Cr-L80 stainless steel
- 4 point bend for SCC testing
- 190 bar / 85°C
- Supercritical CO<sub>2</sub> and formation water
- Continuous injection of CO<sub>2</sub> with 60 ppm-mol O<sub>2</sub>
- Localised corrosion, but no SCC observed



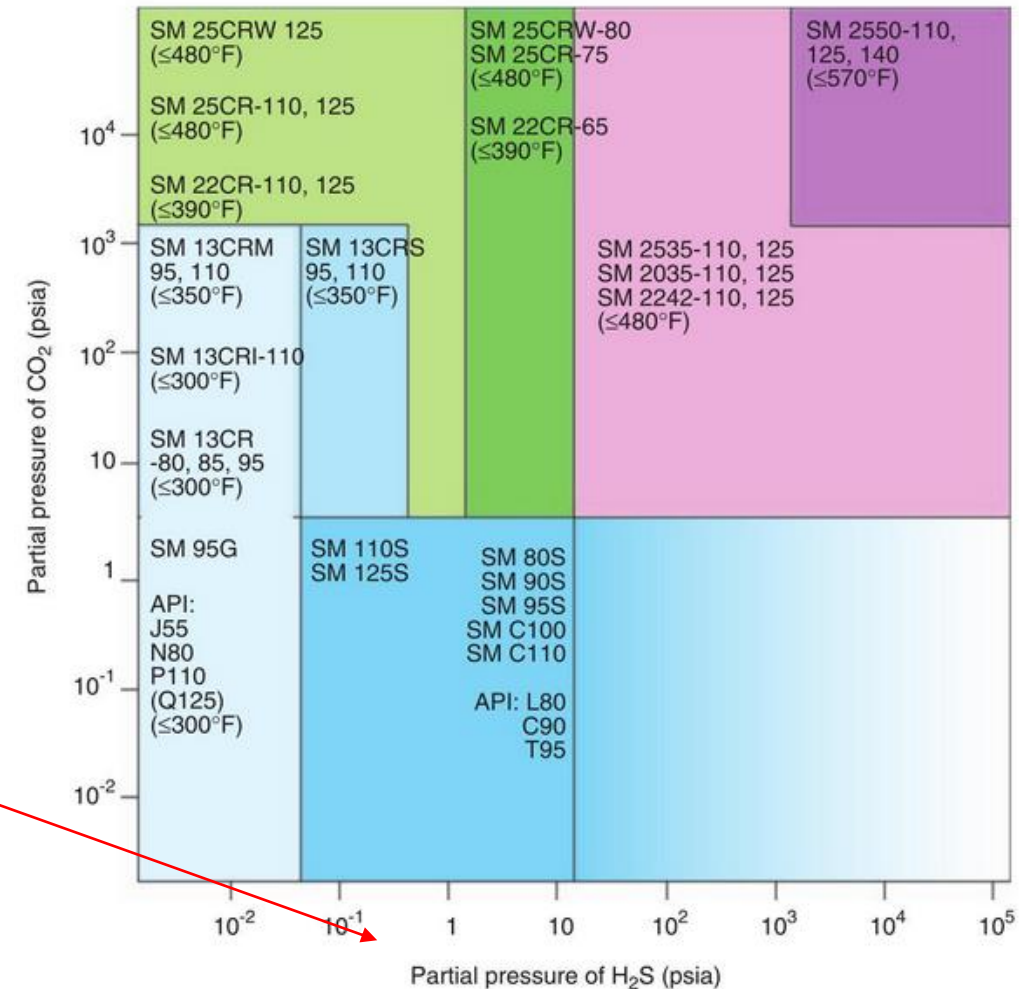
CO<sub>2</sub> phase with  
water condensation



# Topics to be studied further

- 13Cr vs S13Cr vs 22Cr vs 25Cr vs. nickel alloys
- “Evaporation” of formation water  $\Rightarrow$  concentrated salt brine (locally)  $\Rightarrow$  Increased risk of SCC?
- Condensed water  $\Rightarrow$  pH  $\ll$  3?
- Localised corrosion?
- How to assess H<sub>2</sub>S partial pressure limit for sulphide stress cracking in dense phase CO<sub>2</sub> (when H<sub>2</sub>S is not present as a gas)?
- Effect of high CO<sub>2</sub> pressure (fugacity) on cement?

First-pass material selection chart, adopted from Sumitomo Metals \*



\* Bellarby, Chap. 8 Materials selection, in: Well completion design (Amsterdam: Elsevier, 2009) pp. 433-472.

# Thank you for your attention!

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